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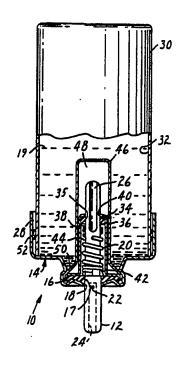
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(54) Title: DEVICE FOR DELIVERING AN AEROSOL

(57) Abstract

A device for delivering an aerosol, comprising: a casing member (14), a valve stem (12), and a diaphragm (16), wherein the diaphragm comprises a thermoplastic elastomer comprising an ethylene/1-butene copolymer. Also disclosed are sealing members comprising such an elastomer and thermoplastic polymer blends, e.g., for use in sealing members of the invention. The devices of the invention are particularly useful with formulations containing 1,1,2-tetrafluoroethane or 1,1,1,2,3,3,3-heptafluoropropane as the propellant.



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- 1 -

DEVICE FOR DELIVERING AN AEROSOL

Technical Field

This invention relates to devices for delivering aerosols. In another aspect this invention relates to sealing members. In yet another aspect this invention relates to sealing members for use in devices for delivering aerosols. This invention also relates to thermoplastic polymer blends.

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Description of the Related Art

The continuing use of aerosol formulations comprising conventional chlorofluorocarbon propellants is being debated due to the suspected role of such propellants in atmospheric depletion of ozone. Accordingly, alternative propellants such as HFC-134a (1,1,2-tetrafluoroethane) and HFC-227 (1,1,1,2,3,3,3-heptafluoropropane) are being developed to replace those conventional propellants thought to contribute to atmospheric ozone depletion.

Containers for aerosol formulations commonly include a rubber valve seal intended to allow reciprocal movement of the valve stem while preventing leakage of propellant from the container. These rubber valve seals are commonly made of thermoset rubbers such as butyl rubber, butadiene-acrylonitrile rubbers, ("Buna") and neoprene (polychloroisoprene), which are compounded with vulcanizing agents prior to being fashioned into valve seals.

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Summary of the Invention

It has been found that some conventional devices for delivering aerosols suffer impaired performance when used in connection with HFC-134a

35 and/or HFC-227. Accordingly, this invention provides a device for delivering an aerosol, comprising: a valve stem, a diaphragm having walls defining a diaphragm aperture, and a casing member having walls defining a

casing aperture, wherein the valve stem passes through the diaphragm aperture and the casing aperture and is in slidable sealing engagement with the diaphragm aperture, and wherein the diaphragm is in sealing engagement with the casing member, the diaphragm material comprising: a thermoplastic elastomer comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, or 1-octene (i.e., the total amount of comonomer in the copolymer is about 5 mole percent to about 20 mole percent).

This invention also provides a metered-dose device for delivering an aerosol that comprises, in 15 addition to the above-discussed valve stem, diaphragm, and casing member, a tank seal having walls defining a tank seal aperture, and a metering tank of a predetermined volume and having an inlet end, an inlet aperture, and an outlet end, wherein the outlet end is 20 in sealing engagement with the diaphragm, the valve stem passes through the inlet aperture and the tank seal aperture and is in slidable engagement with the tank seal aperture, and the tank seal is in sealing engagement with the inlet end of the metering tank, and 25 wherein the valve stem is movable between an extended closed position, in which the inlet end of the metering tank is open and the outlet end is closed, and a compressed open position in which the inlet end of the metering tank is substantially sealed and the outlet 30 end is open to the ambient atmosphere.

In a preferred embodiment the casing member defines a formulation chamber, and in a further preferred embodiment the formulation chamber contains an aerosol formulation comprising a propellant, said propellant comprising 1,1,1,2-tetrafluoroethane, 1,1,1,2,3,3,3-heptafluoropropane, or a mixture thereof.

In another aspect, this invention provides an elastomeric sealing member, e.g., for maintaining a

WO 92/11190 PCT/US91/09726

- 3 -

desired atmosphere in a sealed chamber or for minimizing and/or preventing escape of propellants, such as 1,1,1,2-tetrafluoroethane or 1,1,1,2,3,3,3heptafluoropropane, from a sealed chamber. Such 5 sealing members can be used as appropriate in connection with static seals or dynamic seals, with pressurized or unpressurized systems, and with liquid or dry systems. The sealing member comprises a thermoplastic elastomer comprising a copolymer of about 10 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, and 1-octene. In a preferred embodiment the sealing member is used in a dynamic seal 15 in a pressurized system in order to prevent escape of formulation components, such as 1,1,1,2-tetrafluoroethane or 1,1,1,2,3,3,3heptafluoropropane, from a device for delivering an aerosol.

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This invention also provides thermoplastic polymer blends comprising at least two thermoplastic copolymers, each comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, and 1-octene.

Devices, sealing members, and thermoplastic polymer blends of this invention find use in connection with aerosol formulations involving HFC-134a or HFC-227 as a propellant as well as with formulations containing other propellants such as chlorofluorocarbon propellants. Conventional devices involving thermoset diaphragms of neoprene (polychloroprene), butyl rubber, or butadiene-acrylonitrile "buna" copolymers allow excessive leakage of HFC-134a and HFC-227 from some formulations over time. Particularly in low volume formulations such as pharmaceutical formulations for use in inhalation therapy, this leakage can cause a

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substantial increase in concentration of the active ingredient in the formulation, resulting in delivery of an improper dose. Furthermore, with some formulations the valve stem tends to stick, pause, or drag during 5 the actuation cycle when neoprene or butadiene-acrylonitrile "buna" diaphragms are used. Leakage and smoothness of operation are improved in the devices of the invention compared to like devices involving the conventional diaphragm materials. Hence 10 this invention is particularly desirable for use with aerosol formulations wherein the propellant comprises HFC-134a, HFC-227, or a mixture thereof. Moreover, the thermoplastic elastomers used in the sealing members of the invention, including the thermoplastic polymer 15 blends of the invention, are not compounded with vulcanizing agents and therefore they are free of complications that might arise from contamination by leaching of such vulcanizing agents.

20 Brief Description of the Drawings

The drawing is represented by FIGS. 1 and 2. FIG. 1 is a partial cross-sectional view of one embodiment of a device of the invention, wherein the valve stem is in the extended closed position.

FIG. 2 is a partial cross-sectional view of the embodiment illustrated in FIG. 1, wherein the valve stem is in the compressed open position.

Detailed Description of the Invention

Unless otherwise indicated the copolymers described herein are random copolymers, i.e., the respective monomer units are substantially randomly distributed in the copolymer.

In order to minimize and/or prevent leakage of refrigerants, propellants, or other formulation components, especially propellants such as 1,1,1,2-tetrafluoroethane and 1,1,1,2,3,3,3-heptafluoropropane, from a sealed chamber, this

invention provides thermoplastic elastomeric sealing
members comprising a copolymer of about 80 to about 95
mole percent ethylene and a total of about 5 to about
20 mole percent of one or more comonomers selected from
5 the group consisting of 1-butene, 1-hexene, and 1octene. The thermoplastic elastomer can also contain
minor amounts of conventional polymer additives such as
processing aids, colorants, lubricants, and talc.

Suitable thermoplastic elastomers can be 10 prepared using methods known to those skilled in the art. A preferred thermoplastic elastomer is FLEXOMERTM DFDA 1137 NT7 polyolefin (commercially available from Union Carbide), a thermoplastic elastomer comprising a copolymer of about 91 mole percent ethylene and about 9 15 mole percent 1-butene. This copolymer is said to have a density of 0.905 g/cm3 (ASTM D-1505) and a melt index of 1.0 g/10 min (ASTM D-1238). FLEXOMERTM DFDA 1138 NT polyolefin (commercially available from Union Carbide), a thermoplastic elastomer comprising a copolymer of 20 about 91 mole percent ethylene and about 9 mole percent 1-butene and having a density of 0.900 g/cm3 (ASTM D-1505) and a melt index of 0.4 g/10 min (ASTM D-1238) is also suitable. A further suitable thermoplastic elastomer comprises a copolymer of about 88 mole 25 percent ethylene and about 12 mole percent 1-butene. An example of such a thermoplastic elastomer is FLEXOMER™DEFD 8923 NT polyolefin (obtained on an experimental basis from Union Carbide). This elastomer is said to have a density of 0.890 g/cm^3 (ASTM D-1505),

30 and a melt index of 1.0 g/10 min (ASTM D-1238).

Other exemplary suitable thermoplastic elastomers include:

FLEXOMER™ GERS 1085 NT polyolefin (Union Carbide), comprising a copolymer of about 80 mole
35 percent ethylene and about 20 mole percent 1-butene, having a density of 0.884 g/cm³ (ASTM D-1505) and a melt index of about 0.8 g/10 min (ASTM D 1238);

FLEXOMERTM DFDA 1163 NT7 polyolefin (Union Carbide), comprising a copolymer of about 95 mole percent ethylene, about 1 mole percent 1-butene, and about 4 mole percent 1-hexene, having a density of 5 0.910 g/cm³ (ASTM D 1238) and a melt index of about 0.5 g/10 min (ASTM D 1238); FLEXOMERTM DFDA 1164 NT7 polyolefin (Union Carbide), comprising a copolymer of about 94 mole percent ethylene, about 1 mole percent 1-butene, and about 5 mole percent 1-hexene, having a 10 density of about 0.910 g/cm³ (ASTM D 1505) and a melt index of about 1.0 g/10 min (ASTM D 1238).

FLEXOMER™ 1491 NT7 polyolefin (Union Carbide), comprising a copolymer of about 90 mole percent ethylene and about 10 mole percent 1-butene,
15 having a density of 0.900 g/cm³ (ASTM D 1505) and a melt index of about 1.0 g/10 min (ASTM D 1238);

FLEXOMERTM 9020 NT7 polyolefin (Union Carbide), comprising a copolymer of about 92 mole percent ethylene and about 8 mole percent 1-butene, 20 having a density of 0.905 g/cm³ (ASTM D 1505) and a melt index of about 0.85 g/10 min (ASTM D 1238);

FLEXOMERTM 9042 NT polyolefin (Union Carbide), comprising a copolymer of about 80 mole percent ethylene and about 20 mole percent 1-butene, 25 having a density of 0.900 g/cm³ (ASTM D 1505) and a melt index of about 5.0 g/10 min (ASTM D 1238).

ATTANETM 4602 polyolefin (Dow), comprising a copolymer of about 90 mole percent ethylene and about 10 mole percent 1-octene, having a density of 0.912 30 g/cm³ (ASTM D 792) and a melt index of about 3.3 g/10 min (ASTM D 1238);

ATTANETM 4701 polyolefin (Dow), comprising a copolymer of about 92 mole percent ethylene and about 8 mole percent 1-octene, having a density of 0.912 g/cm³
35 (ASTM D 792) and a melt index of about 1.0 g/10 min (ASTM D 1238).

- 7 -

Blends of two or more of the abovedescribed thermoplastic elastomers in any proportion are also suitable. Preferred thermoplastic polymer blends of the invention include blends of two or more 5 thermoplastic copolymers, each comprising about 80 to 95 mole percent ethylene and about 5 to about 20 mole percent 1-butene. More preferred are blends comprising (i) a copolymer of about 91 mole percent ethylene and about 9 mole percent 1-butene (e.g., FLEXOMER™ DFDA 10 1137 polyolefin), and (ii) a copolymer of about 80 mole percent ethylene and about 20 mole percent 1-butene (e.g., FLEXOMER™ GERS 1085 NT polyolefin). Blends comprising one part by weight of component (i) and about 0.25 to about 4 parts by weight of component (ii) 15 are particularly preferred, especially for use in a dynamic seal and in a pressurized system, e.g., in a metered-dose inhaler.

The polymer blends of the invention can also comprise minor amounts of conventional polymer 20 additives such as processing aids, colorants, lubricants, and talc.

As illustrated in the TABLES below, some of the seal materials and sealing members of the invention are superior to others for use in the dynamic seal of a pressurized aerosol container. Those seal materials that are less than optimal for use in the exemplified systems can nonetheless find use, e.g., in connection with a different general type of drug or a different valve stem than exemplified, as a static seal in a pressurized system, or in a non-pressurized system having a dynamic seal. The TABLES below occasionally contain data that appear somewhat inconsistent with other data (e.g., a single very high standard deviation as in TABLE 17). These aberant results are generally attributable to failure of one or two vials in the test group.

The device of the invention will be described with reference to the Drawing. FIG. 1 shows device 10 comprising valve stem 12, casing member 14, and diaphragm 16. The casing member has walls defining casing aperture 18, and the diaphragm has walls defining diaphragm aperture 17. The valve stem passes through and is in slidable sealing engagement with the diaphragm aperture. The diaphragm is also in sealing engagement with casing member 14. Diaphragm 16 represents a thermoplastic elastomeric sealing member of the invention.

The illustrated embodiment is a device for use with pharmaceutical formulations. The diaphragm in the illustrated embodiment is of a thickness sufficient to form an effective seal with the casing member, preferably about 0.005 inch to about 0.050 inch. It has an outside diameter of about 0.340 inch, and an inside diameter sufficient to form an effective seal with the valve stem. As valve stems having an outside diameter of about 0.110 inch are commonly used, suitable diaphragm inside diameter can be in the range of about 0.080 inch to about 0.105 inch. Diaphragm dimensions suitable for use with other general types of devices can be easily selected by those skilled in the art.

Valve stem 12 is in slidable engagement with diaphragm aperture 17. Helical spring 20 holds the valve stem in an extended closed position as illustrated in FIG. 1. Valve stem 12 has walls defining orifice 22 which communicates with exit chamber 24 in the valve stem. The valve stem also has walls defining channel 26.

In the illustrated embodiment casing member 14 comprises mounting cup 28 and canister body 30 and 35 defines formulation chamber 32. The illustrated embodiment further comprises tank seal 34 having walls defining tank seal aperture 35, and metering tank 36 having inlet end 38, inlet aperture 40, and outlet end

42. The metering tank also has walls defining metering chamber 44 of predetermined volume (e.g., 50 μL).
Outlet end 42 of metering tank 36 is in sealing engagement with diaphragm 16, and valve stem 12 passes
5 through inlet aperture 40 and is in slidable engagement with tank seal 34.

When device 10 is intended for use with a suspension aerosol formulation it further comprises retaining cup 46 fixed to mounting cup 28 and having 10 walls defining retention chamber 48 and aperture 50. When intended for use with a solution aerosol formulation retaining cup 46 is optional. Also illustrated in device 10 is sealing member 52 in the form of an 0-ring that substantially seals formulation 15 chamber 32 defined by mounting cup 28 and canister body 30. Sealing member 52 preferably comprises the elastomeric copolymer described above.

Operation of device 10 is illustrated in FIGS. 1 and 2. In FIG. 1, the device is in the extended closed position. Aperture 50 allows open communication between retention chamber 48 and formulation chamber 32, thus allowing the aerosol formulation to enter the retention chamber. Channel 26 allows open communication between the retention chamber and metering chamber 44 thus allowing a predetermined amount of aerosol formulation to enter the metering chamber through inlet aperture 40. Diaphragm 16 seals outlet end 42 of the metering tank.

FIG. 2 shows device 10 in the compressed open position. As valve stem 12 is depressed channel 26 is moved relative to tank seal 34 such that inlet aperture 40 and tank seal aperture 35 are substantially sealed, thus isolating a metered dose of formulation within metering chamber 44. Further depression of the valve stem causes orifice 22 to pass through aperture 18 and into the metering chamber, whereupon the metered dose is exposed to ambient pressure. Rapid vaporization of the propellant causes the metered dose

to be forced through the orifice, and into and through exit chamber 24. Device 10 is commonly used in combination with an actuator that facilitates inhalation of the resulting aerosol by a patient.

A particularly preferred device of the 5 invention is a metered dose configuration substantially as described above and illustrated in the Drawing. Other particular configurations, metered dose or otherwise, are well known to those skilled in the art 10 are suitable for use with the sealing members of this invention. For example the devices described in U.S. Pat. Nos. 4,819,834 (Thiel), 4,407,481 (Bolton), 3,052,382 (Gawthrop), 3,049,269 (Gawthrop), 2,980,301 (DeGorter), 2,968,427 (Meshberg), 2,892,576 (Ward), 15 2,886,217 (Thiel), and 2,721,010 (Meshberg) (all incorporated herein by reference) involve a valve stem, a diaphragm, and a casing member in the general relationship described herein. Generally any and all sealing members (such as diaphragms, seals, and 20 gaskets) that serve to minimize and/or prevent escape of components, especially propellant, from such assemblies can comprise the above described thermoplastic elastomer.

The devices, sealing members, and polymer

25 blends of the invention can be used in connection with
aerosol formulations involving propellants such as
fluorotrichloromethane, dichlorodifluoromethane, and
1,2-dichlorotetrafluoroethane. However, this invention
finds particular use with aerosol formulations
30 involving a propellant comprising HFC-134a or HFC-227.
Any such formulation can be used. Pharmaceutical
formulations are preferred.

Preferred pharmaceutical formulations generally comprise HFC-134a, HFC-227, or a mixture 35 thereof in an amount effective to function as an aerosol propellant, a drug having local or systemic action and suitable for use by inhalation, and any optional formulation excipients. Exemplary drugs

WO 93/11190 PCT/US91/09726

- 11 -

having local effect in the lung include bronchodilators such as albuterol, formoterol, pirbuterol, and salmeterol, and pharmaceutically acceptable salts and derivatives thereof, and steroids such as

5 beclomethasone, fluticasone, and flunisolide, and pharmaceutically acceptable salts, derivatives, solvates, and clathrates thereof. Exemplary drugs having systemic effect include peptides such as insulin, calcitonin, interferons, colony stimulating factors, and growth factors.

The drug is present in the formulation in an amount sufficient to provide a predetermined number of therapeutically effective doses by inhalation, which can be easily determined by those skilled in the art considering the particular drug in the formulation. Optional excipients include cosolvents (e.g., ethanol, water) and surfactants (e.g., oleic acid, sorbitan esters, polyoxyethylenes, glycols) and others known to those skilled in the art.

A particularly preferred formulation comprises, by weight, 0.40% albuterol sulfate, 0.48% oleic acid, 14.26% absolute ethanol, and 84.86% HFC-134a. Another preferred formulation comprises, by weight, 0.337% beclomethasone dipropionate, 8.0% absolute ethanol, and 91.663% HFC-134a. Yet another preferred formulation comprises, by weight, 0.084% of beclomethasone dipropionate, 8.0% absolute ethanol, and 91.916% HFC-134a.

30 <u>Blend Preparation</u>

Polymer blends of the invention, from which sealing members of the invention can be made, can be prepared by conventional polymer blending techniques well known to those skilled in the art. Those blends exemplified herein were prepared as follows:

Small Scale Compounding

Selected quantities of the blend components are added to a heated 100 mL bowl in a BRABENDERTM laboratory mixer equipped with high shear mixing 5 shafts. The components are mixed under temperature, speed, and time conditions selected according to the characteristics of the components of the blend. After mixing the mixing head is operated in reverse in order to expel the hot, mixed blend, which is compression 10 molded as described below.

Large Scale Compounding

Selected quantities of the blend components are fed at room temperature into a APV Model 2030 TC 15 twin screw extruder via feeders that are calibrated to match the extrusion rate.

Screw speed and extruder temperature are selected according to the characteristics of the components of the blend. The melt is extruded through a 0.63cm (0.25 inch) strand dye having two strand openings. The strands are fed through a water bath, dried, and pelletized with a BERLYN^{MM} Model Pe 112 chopper. The pellets are dried in trays for 1-3 days at about 50°C and extruded into a sheet as described below.

Diaphragm Preparation

Diaphragms of the invention can be prepared by conventional techniques known to those skilled in 30 the art, such as compression molding, extrusion, and injection molding. Those diaphragms exemplified herein were prepared according to the general methods set forth below:

35 Compression Molding

An amount of a selected elastomer sufficient to provide a compression molded sheet of the desired thickness is compression molded between

WO 92/11190 PCT/US91/09726

- 13 -

appropriately spaced aluminum press plates in a CARVERTM
Laboratory Press Model 2696 (Fred S. Carver, Inc.,
Menomonie Falls, Wisconsin) at elevated temperature
(e.g., about 150°C) and pressure (e.g., 170 kPa) and
5 for a time sufficient to form a molded sheet. The
press is then cooled until the mold plates can be
handled. The compression molded sheet is removed from
the mold and hand punched with a die of the desired
size to afford a diaphragm of the invention.

10

Extrusion

A sample of a selected elastomer is fed into the feed throat of a Haake RHEOCORT single-screw extruder fitted with a Haake RHEOMIX three-zone

15 extruder head and equipped with a 1.9 cm (0.75 inch) diameter screw having a 3:1 pitch and a length to diameter ratio of 25:1. Appropriate screw speed and operating temperatures are selected according to the characteristics of the selected elastomer. The melt is extruded through a flat film die, fitted with a shim to provide the desire opening, and over a cooled chrome roller. The thickness of the resulting sheet is controlled by appropriate adjustment of screw speed and speed of the cooled roller. Diaphragms of the invention were hand cut from the sheet with a die of appropriate size.

Injection Molding

The selected elastomer is fed into the feed throat of a Van Dorn 75 ton injection molding machine equipped with a 5 ounce barrel. Operating conditions are selected according to the characteristics of the selected elastomer. The melt is injected into a mold having cavity dimensions appropriate to provide the desired sealing member. Cooling and opening of the mold affords the sealing member.

- 14 -

Test Methods

Sealing members were tested as follows:

Leak Rate

with an aerosol formulation and fitted with a metered dose valve substantially as described and illustrated above and comprising a diaphragm of a selected size and material. The valve is actuated several times in order to assure its function. The mass of the filled device is measured. The filled device is allowed to stand in an upright position under the indicated conditions (30°C unless otherwise indicated) for a period of time, after which time mass is again measured. The loss of mass over time is extrapolated to one year and reported in mg/year.

Valve Delivery

The mass of a filled device is measured.

20 The device is then inverted and actuated one time.

Mass is again determined and the valve delivery is recorded as the difference.

The formulations used in the TABLES below in order to demonstrate the invention are as follows, wherein all parts and percentages are by weight:

Formulation	Albuterol Sulfate (%)	Beclomethasone Dipropionate (%)	Oleic Acid	Ethanol (%)	HFC 134a (%)
A1	0.5		0.1	15	84.4
A2	0.47		0.097	14.24	85.2
A3	0.4		0.5	15	84.1
A4	0.8		0.5	15	83.7
A5	1.2		0.5	15	83.3
A6	0.8		0.5	14.9	83.8
B1		0.164	-	5.87	93.96
82		0.166		6.04	93.78
B3	-	0.44		15	84.56
Q			g•0	15.0	84.5
	Pirbuterol Acetate				HFC-227
ď	68.0	-		10.0	89.11
	Albuterol Sulfate				HFC-227
LA L	0.4	-	.		99.6

Diaphragms of FLEXOMERTM DEFD 8923 NT polyolefin were incorporated in a device substantially as described and illustrated above, and tested alongside devices comprising a neoprene diaphragm or a butadiene-acrylonitrile "buna" resin diaphragm.

Results are shown in TABLE 1 below wherein "RH" designates relative humidity.

	Table 1 - Continued
1	Buna and neoprene diaphragms from American Gasket and Rubber, Chicago, Illinois. "DEFD 8923 NT" designates FLEXOMER" DEFD 8923 NT polyolefin. All DEFD 8923 NT diaphragms were 0.035 inch thick with 0.095 inch inside diameter and 0.34 inch outside diameter. The buna and neoprene diaphragms were 0.038 inch thick with a 0.093 inch inside diameter and a 0.340 inch outside diameter. The valve stem had a 0.110 inch outside diameter.
2	N is the number of vials per group. The first number of the pair is the number of valves whose individual measurements were averaged to give the reported leak rate. The second number of the pair is the number of individual measurements which were averaged to give the reported valve delivery.

The results in TABLE 1 show that, with the designated formulations using HFC-134a as the propellant, leak rates are substantially lower in the devices comprising the diaphragm of the invention than 5 in the devices comprising diaphragms of materials that are commonly used in commercially available metered dose aerosol devices. Only under conditions of thermal stress (40°C, 85% RH) did the devices of the invention have leak rates comparable to those of the comparative 10 devices tested at 30°C. Furthermore, valve delivery is more precise and more constant over time with devices of the invention than in the comparative devices of the prior art. Moreover, while the valves in the comparative devices often stuck, paused, or dragged 15 during actuation, the valves in the devices of the invention generally exhibited smooth operation over the duration of the study.

Diaphragms of the invention of the specified composition and having a thickness of 0.035

20 inch, an outside diameter of 0.34 inch, and various inside diameters were tested with HFC-134a alone and with a model formulation (containing HFC-134a, ethanol, and a surfactant) in devices having either stainless steel ("ss") or DELRINTM acetal resin (DuPont,

25 "plastic") valve stems having a diameter of 0.110 inch. Results are shown in TABLE 2 (FLEXOMERTM DEFD 8923 NT polyolefin), TABLE 3 (FLEXOMERTM DFDA 1137 polyolefin), and TABLE 4 (FLEXOMERTM DFDA 1138 polyolefin) below, wherein each entry represents the mean of seven independent determinations.

Table 2

		Table 2	- continued		
Formulation	(uț) ai	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Value Delivery (mg/actuation) ± SD
134a	0.100	ss plastic	0 20 0	27 ± 4 33 ± 22	58.79 ± 19.27 67.27 ± 0.99 65.07 ± 0.49 65.13 ± 0.73
134a	0.105	ss plastic	909	26 ± 0.81 27 ± 4	65.34 ± 1.80 66.84 ± 0.81 65.13 ± 0.79 65.14 ± 1.85
Q	0.080	ss plastic	0 20 0	147 ± 13 143 ± 14	61.26 ± 1.33 61.61 ± 1.26 60.46 ± 0.80 59.73 ± 0.73
Q	0.085	ss plastic	0000	 140 ± 19 138 ± 6	62.43 ± 1.00 62.71 ± 1.11 61.21 ± 0.75 60.46 ± 0.74
Q .	0.090	ss plastic	2020	149 ± 20 140 ± 12	61.81 ± 0.83 62.07 ± 0.87 61.23 ± 0.56 60.61 ± 0.41

		Table 2 -	Table 2 – continued		
Formulation	ID (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Valve Delivery (mg/actuatio n) ± SD
Q	0.095	ss plastic	0 5 5	 154 ± 8 165 ± 12	63.24 ± 0.73 63.79 ± 0.81 62.26 ± 0.59 62.07 ± 0.49
۵	0.100	ss plastic	50 0 13 0	150 ± 10 167 ± 14	62.99 ± 0.94 63.61 ± 0.97 62.21 ± 1.03 62.39 ± 0.67
Q	0.105	ss plastic	000 0	163 ± 7 171 ± 9	63.79 ± 0.66 64.69 ± 0.64 61.66 ± 1.82 61.77 ± 1.03

PABLE 3

LEAL	LEAK RATE AND VALV ISING FLEXOMER" 113	E DELIVERY WI	TH STAINLESS DIAPHRAGMS H	LEAK RATE AND VALVE DELIVERY WITH STAINLESS STEEL AND PLASTIC VALVE STEMS USING FLEXOMER" 1137 POLYOLEFIN DIAPHRAGMS HAVING VARIOUS INSIDE DIAMETERS	C VALVE STEMS SIDE DIAMETERS
Formulation	on ID (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Valve Delivery (mg/actuation) ± SD
134a	0.080	ល	010	 28.4 ± 3.4	++++
		plastic	O 15	28.6 ± 6.7	62.73 ± 3.40 61.91 ± 3.21
134a	0.085	ល	οư		<u>.,</u> +
		plastic	200	29.6 ± 11.0	61.41 ± 4.20 60.90 ± 7.20
134a	0.090	ស្ល	Ou		58.90 ± 19.00
		plastic	. O iS	27.7 ± 4.2	62.07 ± 3.78 61.23 ± 6.49
134a	0.095	SS	0	1 .	59.83 ± 15.34
		plastic	N O N	25.9 ± 5.9 32.8 + 18.5	66.67 ± 0.67 65.01 ± 0.95 65.16 ± 0.72
)		i

		TABI	TABLE 3 - continued	nued	
Formulation	ID (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Valve Delivery (mg/actuation) ± SD
Q	080.0	នន	OW	163 ± 30.8	59.34 ± 4.75 62.84 ± 0.53
		plastic	0 2	197 ± 34.1	+++
Q	0.085	ss plastic	0 13 0	179 ± 61.8	61.83 ± 1.64 63.13 ± 0.87 59.59 ± 2.41
			2	156 ± 16.4	₩
Q	0.090	ss plastic	ល០ល	169 ± 40.8 225 ± 31.0	60.83 ± 2.39 61.90 ± 2.31 59.04 ± 1.31 60.10 ± 2.66
Q	0.095	នន	010	210 ± 53.0	59.59 ± 4.07 60.00 ± 3.66
		plastic	o s	243 ± 35.9	H +I

TABLE 3

LEAK RATE AND VALVE DELIVERY WITH STAINLESS STEEL AND PLASTIC VALVE STEMS USING FLEXOMER" 1137 POLYOLEFIN DIAPHRAGMS HAVING VARIOUS INSIDE DIAMETERS

		TAB	TABLE 3 - continued	ned	
Formulation	ID (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Valve Delivery (mg/actuation) ± SD
Ω	0.100	ss plastic	0000	187 ± 12.9 282 ± 118	61.49 ± 1.37 61.41 ± 1.25 54.89 ± 3.36 56.14 ± 1.95
۵	0.105	ss plastic	0 10 0	232 ± 30.8	50.81 ± 5.07 53.00 ± 3.28 48.43 ± 2.57 48.51 ± 1.02

C VALVE STEMS SIDE DIAMETERS	Valve Delivery (mg/actuation) ± SD	66.17 ± 56.10 63.03 ± 20.22 62.27 ± 6.85	+ 18 + 17 + 15 + 15	52.64 ± 18.28 68.67 ± 2.12 57.86 ± 15.78 70.34 ± 8.47	57.57 ± 17.59 68.43 ± 1.07 64.84 ±1.69 65.97 ± 2.67	59.70 ± 20.32 67.59 ± 1.95 64.79 ± 0.61 65.53 ± 0.72
TABLE 4 VALVE DELIVERY WITH STAINLESS STEEL AND PLASTIC VALVE STEMS 1138 POLYOLEFIN DIAPHRAGMS HAVING VARIOUS INSIDE DIAMETERS	Leak Rate (mg/yr) ± SD	16.4 ± 2.51	36.8 ± 44.4 15.0 ± 3.9	45.7 ± 43.5 14.8 ± 3.6	22.5 ± 7.3 14.5 ± 3.4	20.3 ± 7.3 21.1 ± 18.8
TABLE 4 TH STAINLESS DIAPHRAGMS H	Time (Weeks)	000	n 0 n o n	_ O	0 0 0	0 0 0 0
DELIVERY WI POLYOLEFIN	Stem	ss plastic	ss plastic	ss plastic	ss plastic	ss plastic
SE.	ID (in)	080.0	0.085	060.0	0.095	0.100
LEAK RATE AND USING FLEXOMER	Formulation	134a	134a	134a	134a	134a

		Tab	Table 4 - continued	panu	
134a	0.105	ss plastic	9 0 0	23.7 ± 3.0 17.4 ± 3.4	65.64 ± 0.90 67.34 ± 0.80 65.11 ± 1.67 68.56 ± 3.86
Formulation	ID (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Valve Delivery (mg/actuation) ± SD
Q	0.080	ss plastic	0 00 0	187 ± 14.3 204 ± 6.2	60.23 ± 0.57 60.90 ± 0.63 58.41 ± 0.52 50.16 ± 22.12
Q	0.085	ss plastic	០១០១	 178 ± 5.4 220 ± 30.4	60.74 ± 1.12 61.30 ± 0.92 58.43 ± 0.45 59.04 ± 2.10
a	060.0	ss plastic	S O S O	237 ± 42.8 258 ± 24.5	60.11 ± 1.36 61.04 ± 1.39 56.87 ± 0.79 56.36 ± 1.01
a	0.095	ss plastic	0 10 0 10	252 ± 40.8 270 ± 21.6	58.37 ± 5.54 60.69 ± 1.98 52.76 ± 6.49 55.26 ± 1.52

		TABI	TABLE 4 - continued	ned	
Formulation	ID (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD	Valve Delivery (mg/actuation) ± SD
Ω	0.100	ss plastic	nono	217 ± 13.3 288 ± 74.6	58.66 ± 0.45 58.60 ± 0.60 56.97 ± 1.37 56.66 ± 1.87
Q	0.105	ss plastic	0 20 0	243 ± 16.3 251 ± 11.0	58.31 ± 0.85 58.51 ± 0.85 57.40 ± 0.98 56.61 ± 0.52

The results in TABLES 2, 3, and 4 show that diaphragms of the invention having various inside diameters afford low leak rates and reproducible valve delivery with stainless steel ("ss") and DELRINTM acetal resin ("plastic") valve stems when used with the designated formulations. Leak rate results with the ethanol-containing formulation, while not as low as with only HFC-134a, compare favorably to the data in TABLE 1 involving buna and neoprene diaphragms.

10 Furthermore, the valves in the devices of the invention generally exhibited smooth operation over the duration of the study.

Diaphragms of the invention prepared from

15 FLEXOMERTMDEFD 8923 NT polyolefin and having an inside diameter of 0.090 inch and various specified thicknesses were tested with HFC-134a alone or with a model formulation (containing HFC-134a, ethanol, and a surfactant) in devices comprising either stainless

20 steel ("ss") or DELRINTM acetal resin ("plastic") valve stems. Results are shown in TABLE 5 below, wherein each entry represents the mean of 7 independent

determinations.

RIOUS THICKNESSES	Leak Rate (mg/yr) ± SD	25.8 ± 4.0 24.6 ± 3.9	27.3 ± 4.3 48.5 ± 66.0	24.5 ± 2.0 22.2 ± 3.5	24.5 ± 6.5 24.5 ± 11	21.9 ± 2.5 20.0 ± 1.6
DIAPHRAGMS OF VA	Time (Weeks)	0 10 0 10	0 20 0	0 0 0 0	0 20 20	0 10 0 10
TABLE 5 LEAK RATE USING FLEXOMER" 8923 NT POLYOLEFIN DIAPHRAGMS OF VARIOUS THICKNESSES	Stem	ss plastic	ss plastic	ss plastíc	ss plastic	ss plastic
	Thickness (in)	0.038	0.035	0.029	0.025	0.020
LEAK RATE	Formulation	134a	134a	134a	134a	134a

	Leak Rate (mg/yr) ± SD	22.2 ± 2.6	50.0 ± 2.6	46.7 ± 38.7	16.5 ± 2.3	200 ± 17	217 ± 14	185 ± 8.7	209 ± 12	182 + 2.5	201 ± 12
TABLE 5 - continued	Time (Weeks)	0 M 0	0	ວທ	0 5	0 10	2 0	ou	5	0 ư	n O G
	Stem		plastic	ທ	plastic	88	plastic	SS	plastic	SS	plastic
	Thickness (in)	0.015		0.010		0.038		0.035		0.029	
	Formulation	134a		134a		Q		Q		۵	-

		TABLE 5 - continued	ed	
Formulation	Thickness (in)	Stem	Time (Weeks)	Leak Rate (mg/yr) ± SD
Ω	0.025	ss plastic	_ O M O M	176 ± 6.4 210 ± 4.8
Q	0.020	ss plastic	0 20 0 0	190 ± 6.5
Q	0.015	ss plastic	0 0 5	182 ± 7.8 196 ± 6.4
Q	0.010	ss plastic	0 0 0 0	180 ± 5.4 201 ± 20

WO 92/11190 PCT/US91/09726

- 33 -

The results in TABLE 5 show that with the designated formulations leak rate is lower in devices comprising a diaphragm of the invention than in devices such as those tested in connection with TABLE 1 above comprising a buna or neoprene diaphragm. TABLE 5 also shows that relatively thin diaphragms can be used with little or no loss of performance.

In the TABLES that follow, the inside diameter of the diaphragms (ID) is given in thousandths of an inch, "pl" represents a valve stem made of DELRIN™ acetal resin (DuPont) having a diameter of 0.110 inch, and "N" refers to the number of independent determinations used in calculating the leak rate and valve delivery values.

Diaphragms of the invention were prepared by compression molding, injection molding, and extrusion from FLEXOMER™ GERS 1085 NT polyolefin and tested with the formulations indicated in TABLES 6-8 below.

	Valve Delivery (mq/actuation)	56.81 ± 0.74 57.18 ± 0.82	55.94 ± 3.64 58.74 ± 1.26	58.09 ± 6.45 59.74 ± 2.92	58.40 ± 0.95 59.33 ± 1.44	58.41 ± 1.46 60.40 ± 2.78	55.94 ± 7.25 62.52 ± 3.77	55.91 ± 1.48 55.62 ± 0.68	54.22 ± 4.63 56.71 ± 2.22	57.42 ± 4.56 58.67 ± 2.13
GERS 1085 NT POLYOLEFIN	Leak Rate (mq/yr)	243 ± 10	247 ± 10	240 ± 9	231 ± 12	227 ± 8	224 ± 8	270 ± 6	 270 ± 11	 265 ± 16
TABLE 6 COMPRESSION MOLDED FLEXOMER* GERS 1085	Z	14	14	14	14	14	14	14	14	14
	Time (Weeks)	0	0 9	9	0	0	0	0	0	0
	Stem	ល	SS	SS	SS	SS	SS	pl	Įď	рl
	ID	80	85	90	95	100	105	80	85	96
	Formulation	A1								

		TABI	TABLE 6 - continued	inued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mq/yr)	Valve Delivery (mg/actuation)
	95	pl	9	14	 260 ± 8	56.10 ± 4.14 58.67 ± 1.72
	100	ρŢ	9	14	256 ± 14	58.73 ± 3.30 60.96 ± 3.72
	105	p1	9	14	 243 ± 11	57.96 ± 3.17 61.50 ± 1.35

	Valve Delivery (mq/actuation)	57.70 ± 1.06 59.17 ± 1.12	56.51 ± 2.98 60.21 ± 2.34	58.87 ± 1.85 58.70 ± 0.64	58.12 ± 0.54 59.48 ± 2.75	55.49 ± 2.52 55.92 ± 1.81	56.33 ± 0.34 56.56 ± 0.24	56.21 ± 1.23 56.72 ± 0.42	55.35 ± 2.74 56.54 ± 0.99	62.18 ± 0.92 63.24 ± 1.26	61.93 ± 0.50 64.20 ± 3.20
1085 NT POLYOLEFIN	Leak Rate (mq/yr)	263 ± 8	275 ± 10	286 ± 12	 269 ± 11	267 ± 9	 284 ± 11	 286 ± 10	282 ± 11	231 ± 16	232 ± 11
	N	10	10	10	10	10	10	10	10	10	10
TABLE 7 FLEXOMER™ GERS	Time (Weeks)	0	09	0	0	0	09	0	0	9	0 9
MOLDED	Stem	នន	ល	ស	SS	pl	pl	pl	pl	និន	ល
INJECTION	ID	84	88	94	66	84	88	94	99	84	88
	Formulation	A1								B1	

		TA	TABLE 7 - continued	itinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	88	pl	9	10	 246 ± 10	60.29 ± 0.78 60.57 ± 0.45
	94	pl	0	10	 251 ± 10	60.75 ± 0.96 60.73 ± 0.64
	66	pl	9	10	 264 ± 22	59.43 ± 3.11 60.46 ± 0.45

				W						-	
	Valve Delivery (mg/actuation)	58.26 ± 2.17 57.76 ± 0.96	57.49 ± 2.24 57.99 ± 2.23	58.66 ± 1.91 58.01 ± 0.66	57.29 ± 2.97 58.30 ± 1.11	58.49 ± 1.64 58.16 ± 0.77	57.97 ± 1.40 57.99 ± 1.10	55.91 ± 0.69 55.50 ± 0.66	55.18 ± 1.41 55.25 ± 0.48	56.38 ± 0.66 55.54 ± 0.53	56.68 ± 0.71 55.67 ± 0.58
POLYOLEFIN	Leak Rate (mq/yr)	279 ± 9	 274 ± 15	 274 ± 15	282 ± 18	284 ± 18	307 ± 11	270 ± 14	275 ± 8	277 ± 12	284 ± 14
1085 NT PO	N	10	10	10	10	10	10	10	10	10	10
GERS	Time (Weeks)	09	9	0	9	9	9	09	0	0	0
EXTRUDED FLEXOMER	Stem	SS	SS	SS	SS	SS	SS	pl	pl	ľď	pl
EXTR	ID	80	85	06	95	100	105	80	85	06	95
	Formulation	A2		·							

		Ta	Table 8 - co	continued		
	100	SS	0 9	10	 284 ± 18	58.49 ± 1.64 58.16 ± 0.77
	105	ល	0 9	10	307 ± 11	57.97 ± 1.40 57.99 ± 1.10
	80	pl	9	10	270 ± 14	55.91 ± 0.69 55.50 ± 0.66
	85	pl	0	10	 275 ± 8	55.18 ± 1.41 55.25 ± 0.48
	06	pl	9	10	27. ± 772	56.38 ± 0.66 55.54 ± 0.53
	95	pl	9	10	 284 ± 14	56.68 ± 0.71 55.67 ± 0.58
	100	pl	9	10	 282 ± 13	56.37 ± 0.70 55.41 ± 0.51
	105	pl	0	10	 318 ± 25	56.38 ± 0.65 55.56 ± 0.64
A3	80	SS	9	10	232 ± 18	58.35 ± 0.74 not measured
	85	SS	9	10	 233 ± 20	58.35 ± 1.00 57.96 ± 0.92

		TAI	TABLE 8 - con	continued		
Formulation	ID	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mq/actuation)
А3	90	SS	09	10	247 ± 62	57.60 ± 2.61 57.85 ± 0.87
	95	នន	09	10	226 ± 22	58.82 ± 0.73 58.41 ± 0.74
	100	SS	0 9	10	231 ± 23	58.97 ± 0.83 58.59 ± 0.65
	105	នន	09	10	253 ± 22	58.87 ± 1.02 not measured
	80	pl	0	10	 236 ± 13	55.98 ± 0.55 54.97 ± 0.35
	85	pl	0	10	 239 ± 15	56.17 ± 0.50 54.65 ± 0.72
	90	pl	0	10	230 ± 9	56.27 ± 0.55 55.01 ± 0.58
	95	pl	0	10	239 ± 20	56.78 ± 1.80 55.93 ± 0.52
	100	pl	0	10	231 ± 11	57.38 ± 0.69 55.95 ± 0.74
	105	pl	9	10	245 ± 16	57.34 ± 0.70 55.56 ± 0.49

				<u>-</u>			7				
	Valve Delivery (mg/actuation)	60.32 ± 3.80 62.60 ± 0.94	62.49 ± 1.02 63.34 ± 0.78	62.68 ± 0.89 63.16 ± 0.71	62.60 ± 0.66 64.36 ± 3.29	63.39 ± 2.36 65.12 ± 2.70	64.08 ± 1.67 64.39 ± 0.85	61.20 ± 3.22 59.90 ± 0.33	60.15 ± 1.02 60.05 ± 0.71	$60.95 \pm 2.00 \\ 60.14 \pm 0.68$	54.61 ± 19.10
	Leak Rate (mg/yr)	157 ± 16	190 ± 60	153 ± 11	 156 ± 10	 155 ± 10	155 ± 7	 158 ± 9	156 ± 11	 158 ± 28	1 2 4 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
continued	N	10	10	10	10	10	10	10	10	10	10
TABLE 8 - con	Time (Weeks)	0 9	00	0 9	0	0	9	9	0	0	0
TA	Stem	w w	ស	ស	ល	ស	នន	pl	pl	pl	pl
	ID	80	85	06	95	100	105	80	85	90	95
	Formulation	B2	·								

		TAI	TABLE 8 - con	- continued		
Formulation	ID	Stem	Time (Weeks)	z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
B2	100	ន	0	1.0	 155 ± 10	63.39 ± 2.36 65.12 ± 2.70
	105	និ	9	10	7 ± 351	64.08 ± 1.67 64.39 ± 0.85
	80	pl	9	10	6 ∓ 851	61.20 ± 3.22 59.90 ± 0.33
	85	pl	9	10	11 ∓ 951	60.15 ± 1.02 60.05 ± 0.71
	90	pı	9	10	158 ± 28	60.95 ± 2.00 60.14 ± 0.68
	95	pl	0	10	158 ± 7	54.61 ± 19.10 60.94 ± 0.59
	100	pl	0	10	153 ± 10	61.05 ± 1.37 61.71 ± 2.26
	105	pl	0	10	 154 ± 9	60.85 ± 0.62 60.71 ± 0.66

The results in TABLES 6-8 show that these diaphragms of the invention exhibit acceptable leak rate and valve delivery variability when used with the indicated formulations, regardless of the method of preparation or the valve stem material.

Diaphragms of the invention were prepared by injection molding and by compression molding from FLEXOMER™ DFDA 1137 NT 7 polyolefin and tested with the formulations indicated in TABLES 9A and 9B below.

TABLE 9 A INJECTION MOLDED FLEXOMER" DFDA 1137 NT 7 POLYOLEFIN

		•			
ID Stem	Stem	 Time (Weeks)	Z	Leak Rate (mq/yr)	Valve Delivery (mg/actuation)
84 ss	នន	 0 9	10	297 ± 41	61.51 ± 2.04 61.79 ± 1.78
88	ន	 0	10	298 ± 35	59.56 ± 0.80 61.28 ± 3.39
94 ss	ល	0	10	312 ± 18	61.57 ± 3.81 66.49 ± 7.58
98 ss	នន	 9	10	289 ± 17	61.88 ± 5.25 63.31 ± 7.20
84 pl	pl	 9	10	298 ± 32	60.88 ± 2.38 59.47 ± 1.12
88 pl	pl	09	10	288 ± 35	59.68 ± 1.80 59.33 ± 1.25
94 pl	рl	 0	10	303 ± 23	59.14 ± 1.05 61.38 ± 4.29
98 p1	pl	 09	10	292 ± 16	58.81 ± 2.06 60.56 ± 1.75

TABLE 9 B

COMPRESSION MOLDED FLEXOMER" DFDA 1137 NT 7 POLYOLEFIN

The results in TABLES 9A and 9B show that these diaphragms of the invention exhibit acceptable leak rate (which increases over time) and valve delivery variability when used with the indicated formulations. Little difference is seen between valve stem types or between injection molded diaphragms and compression molded diaphragms. A similar increase in leak rate was observed over time when compression molded FLEXOMERTM DFDA 1138 NT polyolefin was used as the diaphragm material with formulations A4 and B3.

Diaphragms of the invention were prepared from FLEXOMERTM DFDA 1163 NT7 polyolefin and tested with the formulations indicated in TABLE 10 below.

				-							
	Valve Delivery (mg/actuation)	60.09 ± 0.81 60.31 ± 0.68	60.28 ± 0.78 60.46 ± 0.86	60.31 ± 1.20 60.56 ± 0.90	59.44 ± 1.33 60.18 ± 0.94	59.64 ± 1.35 60.09 ± 1.15	60.01 ± 0.85 59.79 ± 0.76	58.96 ± 0.61 not measured	59.44 ± 0.56 58.07 ± 1.80	59.22 ± 0.65 58.51 ± 0.57	58.96 ± 0.65 58.34 ± 0.76
NT 7 POLYOLEFIN	Leak Rate (mq/yr)	259 ± 9	279 ± 14	278 ± 17	299 ± 20	394 ± 341	293 ± 22	286 ± 72	275 ± 13	295 ± 45	300 ± 23
10 DFDA 1163 N	N	14	14	14	14	14.	14	14	14	14	14
TABLE 10 FLEXOMER DFD	Time (Weeks)	09	0	0	9	0	0	09	0	0	9
	Stem	ល	w w	SS	ន	នន	នន	pl	pl	pl	pl
COMPRESSION MOLDED	ID	80	85	06	95	100	105	80	85	90	95
Ö	Formulation	A1						-			

		Tab	Table 10 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	Įď	9	14	315 ± 34	58.73 ± 0.70 58.73 ± 2.18
	105	ρŢ	9	14	 899 ± 2183	58.19 ± 0.67 58.08 ± 1.43

WO 92/11190 PCT/US91/09726

- 49 -

The results in TABLE 10 show that these diaphragms of the invention exhibit higher but generally acceptable leak rates and valve delivery variability when used with the indicated formulations, regardless of valve stem type. However, increasing inside diameter appears to increase leak rate with the plastic valve stem.

Diaphragms of the invention were prepared from FLEXOMERTM DFDA 1164 NT7 polyolefin and tested with the formulations indicated in TABLES 11-13 below.

	Valve Delivery (mg/actuation)	60.57 ± 0.62 60.74 ± 0.56	61.04 ± 0.99 61.30 ± 0.88	61.16 ± 0.77 58.94 ± 7.77	$61.26 \pm 0.73 \\ 61.74 \pm 0.80$	60.19 ± 0.65 60.93 ± 0.90	60.60 ± 0.52 60.90 ± 0.67	59.82 ± 0.92 59.23 ± 0.71	59.90 ± 0.78 59.44 ± 0.75	60.02 ± 1.04 59.64 ± 1.63	60.20 ± 1.05 59.76 ± 1.38
NT 7 POLYOLEFIN	Leak Rate (mg/yr)	421 ± 195	338 ± 108	357 ± 264	628 ± 634	458 ± 229	478 ± 263	276 ± 50	264 ± 19	 262 ± 16	268 ± 17
1164	N	14	14	14	14	14	14	14	14	14	14
TABLE 11 FLEXOMER" DFDA	Time (Weeks)	9	9	9	9	0	0 9	0	0	0	9
	Stem	SS	ន	នន	SS	ន	SS	pl	pl	pl	pl
COMPRESSION MOLDED	ID	80	85	06	95	100	105	80	85	06	95
00	Formulation	A1									

		Tab	Table 11 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	pl	0	14	380 ± 385	58.68 ± 1.74 58.69 ± 2.87
	105	pl	9	14	308 ± 48	58.41 ± 1.94 59.73 ± 1.84

								- T	T		
	Valve Delivery (mg/actuation)	62.34 ± 2.83 69.99 ± 7.80	63.45 ± 4.87 69.30 ± 9.12	65.22 ± 6.21 69.09 ± 7.02	$65.51 \pm 5.42 \\ 81.53 \pm 25.99$	62.62 ± 2.15 60.99 ± 4.02	60.67 ± 2.76 59.67 ± 3.38	64.18 ± 5.65 60.67 ± 2.30	62.19 ± 3.86 not measured	69.83 ± 6.84 76.36 ± 8.94	70.33 ± 5.42 74.86 ± 6.29
TABLE 12 FLEXOMER" DFDA 1164 NT 7 POLYOLEFIN	Leak Rate (mg/yr)	305 ± 35	301 ± 23	304 ± 14	308 ± 19	428 ± 334	350 ± 110	582 ± 397	327 ± 23	284 ± 22	260 ± 33
1164 NT	×	10	10	10	10	10	10	10	10	10	10
TABLE 12 XOMER" DFDA	Time (Weeks)	0	09	9	09	0 9	09	0 9	0	09	09
MOLDED FLE	Stem	. v	នន	ស :	n N	pl	рl	pl	pl	SS	នួន
INJECTION MOLDED	ID	84	88	94	66	84	88	94	66	84	88
1	Formulation	A1								B1	

		TAB	TABLE 12 - continued	ntinued		
Formulation	αI	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	94	SS	0	10	273 ± 33	67.83 ± 4.70 71.89 ± 4.32
	66	ន	0	10	 255 ± 19	69.73 ± 4.97 81.76 ± 8.71
B1	84	pl	0	10	 286 ± 29	69.04 ± 5.87 69.72 ± 6.85
	88	pl	9	10	 629 ± 1064	68.16 ± 6.78 69.30 ± 6.70
	94	pl	0	10	 292 ± 38	66.15 ± 2.89 67.20 ± 8.22
,	99	pl	0 9	10	491 ± 654	69.45 ± 7.39 70.29 ± 7.77

									-		-
	Valve Delivery (mg/actuation)	66.90 ± 0.37 67.05 ± 0.42	65.26 ± 1.26 63.81 ± 1.61	65.10 ± 0.96 66.55 ± 0.76	65.67 ± 1.30 66.53 ± 0.90	66.58 ± 2.91 66.39 ± 1.54	65.03 ± 2.90 67.02 ± 1.61	64.77 ± 2.20 64.29 ± 1.45	63.55 ± 1.17 63.53 ± 1.07	63.40 ± 0.57 64.45 ± 1.60	63.43 ± 0.63 64.70 ± 1.85
NT 7 POLYOLEFIN	Leak Rate (mq/yr)	306 ± 154	321 ± 271	232 ± 122	425 ± 292	757 ± 380	698 ± 499	184 ± 29	211 ± 23	198 ± 21	226 ± 24
	Z	10	10	10	10	10	10	10	, 10	10	10
TABLE 13 FLEXOMER" DFDA 1164	Time (Weeks)	9	09	9	0	0.9	0	0	0	0 9	0 0
ED FLEXOME	Stem	88	SS	SS	SS	ល	ន	pl	pl	pl	рl
EXTRUDED	ID	80	85	90	98	100	105	80	85	90	95
	Formulation	B2									

		TAB	TABLE 13 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	pl	0	10	 341 ± 388	63.59 ± 0.71 66.27 ± 4.49
	105	рĵ	0 9	10	 226 ± 29	63.17 ± 0.85 69.72 ± 8.48

The results in TABLES 11-13 show that these diaphragms of the invention exhibit higher but generally suitable leak rate and valve delivery variability when used with the indicated formulations.

- 5 Valve delivery is least variable for the compression molded diaphragms. With the extruded diaphragms leak rate with the beclomethasone dipropionate formulation is improved when a plastic valve stem is used.
- Diaphragms of the invention were prepared

 10 from FLEXOMERTM DEFD 1491 NT7 polyolefin and tested with
 the formulations indicated in TABLE 14 below.

	Valve Delivery (mg/actuation)	58.69 ± 1.15 58.86 ± 1.46	+++	59.13 ± 0.97 59.59 ± 0.96	++	+1+1	+1+1	++++	58.22 ± 0.54 57.66 ± 0.64	+1+1	58.02 ± 0.84 57.68 ± 0.58
NT 7 POLYOLEFIN	Leak Rate (mq/yr)	 275 ± 26	277 ± 23	768 ± 20	284 ± 26	279 ± 19	+1		283 ± 28	269 ± 8	276 ± 13
<u>14</u> DEFD 1491 N	N	14	14	14	14	14	14	14	14	14	14
TABLE 14 FLEXOMER" DEI	Time (Weeks)	0	0	0	9	0	0	0	0	0	0
RESSION MOLDED FL	Stem	SS	SS	នន	SS	នន	SS	рĵ	pl	pl	pl
COMPRESSIO	ID	80	85	06	95	100	105	80	85	90	95
Ö	Formulation	A1									

			TABLE 14	4		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
·	100	pl	9	14	 281 ± 17	57.72 ± 0.74 57.26 ± 0.88
	105	ιď	9 0	14	276 ± 19	58.29 ± 0.65 56.21 ± 3.22

- 59 -

The results in TABLE 14 show that these diaphragms of the invention exhibit acceptable leak rates and valve delivery variability when used with the indicated formulations.

Diaphragms of the invention were prepared from FLEXOMER^m DFDA 9020 NT7 polyolefin and tested with the formulations indicated in TABLES 15-16.

[
	Valve Delivery (mq/actuation)	58.82 ± 3.64 59.68 ± 0.77	59.57 ± 1.24 59.71 ± 0.84	59.54 ± 0.73	59.91 ± 1.15 59.51 ± 0.64	60.09 ± 0.84 60.83 ± 4.08	59.99 ± 1.31 60.04 ± 0.92	57.99 ± 1.83 57.30 ± 2.62	58.18 ± 0.89 57.77 ± 0.63	59.11 ± 0.69 58.42 ± 0.68	58.54 ± 0.80 57.79 ± 0.63
POLYOLEFIN	Leak Rate (mq/yr)	262 ± 14	278 ± 22	 271 ± 20	296 ± 22	289 ± 17	283 ± 15	281 ± 41	302 ± 20	291 ± 21	354 ± 103
15 9020 NT 7 P	N	14	14	14	14	14	14	14	14	14	14
	Time (Weeks)	9	9	0 9	0	0	09	0	0	0	0
TABLE EXTRUDED FLEXOMER" DFDA	Stem	នន	SS	ល	SS	SS	ន	pl	pl	pl	p1
EXTRUE	ID	80	85	06	95	100	105	80	.85	9.0	95
	Formulation	A2								-	

		Tab	Table 15 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	pl	0 9	14	319 ± 16	58.59 ± 1.09 58.58 ± 2.84
	105	p1	9	14	319 ± 30	58.20 ± 0.74 57.99 ± 1.23

	Valve Delivery (mg/actuation)	59.43 ± 0.70 58.82 ± 0.74	59.27 ± 0.78 58.76 ± 0.41	59.44 ± 2.03 58.67 ± 0.83	59.03 ± 0.73 58.95 ± 0.79	58.51 ± 2.49 58.06 ± 2.04	59.00 ± 1.27 58.63 ± 1.98	65.57 ± 1.14 66.66 ± 0.86	65.75 ± 0.80 66.67 ± 1.42	65.56 ± 1.30 66.74 ± 0.80	66.35 ± 2.19 67.03 ± 0.93
N7 POLYOLEFIN	Leak Rate (mg/yr)	 not measured	 240 ± 15	 230 ± 18	236 ± 17	 243 ± 76	304 ± 253	221 ± 90	338 ± 228	471 ± 482	424 ± 381
16 PEDA 9020 P	N	14	14	14	14	14	14	14	14	14	14
TABLE 16 FLEXOMER™ DE	Time (Weeks)	0	0 0	0	0	0	0	0	0	0	0
RESSION MOLDED F	Stem	pl	pl	pl	pl	рl	pl	ស	SS	នន	ន
COMPRESSIC	ID	80	85	90	95	100	105	80	85	90	95
)	Formulation	A3						B2			

		Tak	Table 16 - co	continued		
Formulation	ID	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	ន	0	14	564 ± 490	65.72 ± 0.67 66.40 ± 0.60
	105	SS	0	14	 671 ± 622	66.40 ± 1.32 66.43 ± 1.14
B2	80	pl	0	14	 174 ± 18	63.26 ± 0.48 63.41 ± 0.50
	85	pl	0	14	186 ± 21	62.93 ± 0.86 63.80 ± 0.78
	06	pl	0 9	14	179 ± 13	63.50 ± 0.97 64.24 ± 0.89
	95	pl	0	14	175 ± 10	62.82 ± 1.71 64.58 ± 1.13
	100	pl	0 9	14	174 ± 33	62.60 ± 2.83 63.43 ± 1.69
	105	pl .	0	14	 168 ± 18	63.51 ± 1.47 66.57 ± 8.55

The results in TABLES 15 and 16 show that the extruded and compression molded diaphragms have valve delivery and leak rate especially suitable for use with a polar ionized drug (albuterol sulfate), 5 while the compression molded diaphragms used with the plastic valve stem are particularly suitable for use with a steroid formulation (beclomethasone dipropionate).

Diaphragms of the invention were prepared from FLEXOMERTM DEFD 9042 NT polyolefin and tested with the formulations indicated in TABLES 17-19 below.

	Valve Delivery (mg/actuation)	61.59 ± 1.50 63.14 ± 0.88	60.77 ± 2.30 63.18 ± 1.04	58.94 ± 4.45 60.86 ± 2.81	59.81 ± 2.42 60.46 ± 2.22	44.61 ± 13.56 50.75 ± 5.58	58.16 ± 1.23 59.01 ± 0.82	61.14 ± 0.59 61.29 ± 0.66	59.96 ± 1.28 60.41 ± 0.88	57.35 ± 1.68 55.71 ± 5.71	54.95 ± 2.84 55.44 ± 3.48
POLYOLEFIN	Leak Rate (mq/yr)	270 ± 20	249 ± 22	252 ± 19	 251 ± 21	270 ± 33	187 ± 25	 268 ± 22	265 ± 14	339 ± 141	286 ± 30
9042 NT	z	14	14	14	14	14	14	14	14	14	14
TABLE 17	Time (Weeks)	3	9	0	0 9	9	9	0	0	0	0 0
COMPRESSION MOLDED	Stem	ន	ន	SS	SS	SS	SS	pl	pl	pl	pl
COMPRES	ΙD	80	85	06	95	100	105	80	85	90	95
	Formulation	A1									

		TAB	TABLE 17 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	рl	0	14	 304 ± 24	55.37 ± 4.10 56.25 ± 3.33
	105	p1	0	14	 208 ± 31	57.83 ± 0.67 60.14 ± 2.62

	1								
	Valve Delivery (mg/actuation)	61.21 ± 1.86 61.10 ± 1.26	60.89 ± 1.62 60.50 ± 3.44	61.18 ± 2.86 60.65 ± 1.09	58.47 ± 1.01 60.59 ± 1.20	59.40 ± 1.27 60.35 ± 1.16	59.94 ± 1.22 60.97 ± 0.69	57.99 ± 0.72 57.71 ± 0.52	58.12 ± 0.98 53.93 ± 15.53
8 9042 NT POLYOLEFIN	Leak Rate (mg/yr)	289 ± 85	 281 ± 63	294 ± 64	 252 ± 18	 255 ± 12	 437 ± 375	 246 ± 9	 262 ± 10
142 NT PC	Z	14	14	14	14	14	14	14	14
TABLE 18 IER [™] DEFD 90	Time (Weeks)	0	9	0	9	9	9	9	9
TABLE 1 EXTRUDED FLEXOMER [™] DEFD	Stem	SS	SS	SS	SS	SS	SS	pl	pl
EXTR	ID	80	85	06	95	100	105	80	85
	Formulation	A2							

·		TAB	TABLE 18 - continued	ntinued		
Formulation	ΟΊ	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	06	pl	0	14	 262 ± 16	57.88 ± 0.85 57.40 ± 1.79
	95	pı	9	14	 256 ± 14	58.15 ± 1.10 57.88 ± 1.44
	100	τď	9	14	 268 ± 26	57.06 ± 1.40 57.31 ± 0.79
	105	þl	0	14	 316 ± 94	56.21 ± 1.68 59.84 ± 6.31

	Valve Delivery (mg/actuation)	60.40 ± 1.70 67.20 ± 8.78	60.40 ± 1.28 75.56 ± 25.41	61.60 ± 2.07 66.63 ± 13.64		+1+1	65.99 ± 12.41 60.32 ± 4.43	61.20 ± 3.64 60.28 ± 3.42	61.22 ± 4.87 59.40 ± 3.19
<u>19</u> DEFD 9042 NT POLYOLEFIN	Leak Rate (mg/yr)	282 ± 13	 282 ± 13	282 ± 14	297 ± 16	272 ± 14	 286 ± 22	284 ± 18	 291 ± 8
7D 9042 N	N	10	10	10	10	10	10	10	10
	Time (Weeks)	0	9	09	0	9	9	9	9
TABLE JECTION MOLDED FLEXOMER"	Stem	SS	ន	SS	88	p1	pl	pl	pl
INJECTIO	ID	84	88	94	66	84	88	94	66
1	Formulation	A2							

		TAB	TABLE 19 - continued	ntinued		
Formulation	dī	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
B2	84	នន	0	10	198 ± 11	70.48 ± 10.53 69.54 ± 3.92
	88	នន	9	10	 202 ± 18	64.71 ± 1.23 71.80 ± 7.10
	94	ន	0 9	10	 199 ± 18	65.01 ± 2.66 86.26 ± 31.64
	66	នន	9	10	208 ± 30	66.80 ± 5.98 80.90 ± 34.78
вг	84	ρĵ	9	10	207 ± 15	64.81 ± 3.57 63.90 ± 1.47
	88	pl	9	10	 200 ± 10	63.96 ± 4.78 64.46 ± 2.31
	94	pl	0 9	10	 207 ± 14	65.17 ± 4.19 69.00 ± 7.64
	66	pl	0	10	219 ± 22	65.27 ± 3.27 78.26 ± 40.98

- 71 -

The results in TABLES 17-19 show that in this instance compression molded and extruded diaphragms generally perform better than the injection molded diaphragms with these formulations.

Diaphragms of the invention were prepared from polymer blends of the invention as set forth in TABLES 20-25 (parts and percentages are by weight) and tested with the formulations indicated in said TABLES.

(25/75)	Valve Delivery (mg/actuation)	55.70 ± 1.91 56.55 ± 0.62	54.38 ± 6.57 57.31 ± 0.88	56.08 ± 1.96 57.22 ± 0.96	56.00 ± 1.08 56.97 ± 1.09	55.54 ± 1.03 56.91 ± 0.84	56.45 ± 0.89 57.49 ± 0.62	54.29 ± 1.45 54.81 ± 0.41	54.93 ± 0.89 55.79 ± 0.71	55.63 ± 0.89 55.39 ± 0.60
NT 7/GERS 1085 NT (25	Leak Rate (mg/yr)	 271 ± 18	 261 ± 12	 264 ± 10	 264 ± 15	 266 ± 12	278 ± 19	 259 ± 12	 271 ± 18	264 ± 7
	Z	10	10	10	10	10	10	10	10	10
TABLE 20 DFDA 1137	Time (Weeks)	9	9	9	9	9	9	9	0	0
D POLYMER BLEND.	Stem	នន	ល	ល	នន	SS	នន	pl	pl	pl
OLDED POL	ID	80	85	90	98	100	105	80	85	06
COMPRESSION MOLDE	Formulation	A1	-			-				

		TABLE	20 -	continued		
Formulation	ΩI	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	92	pl	0 9	10	 271 ± 13	55.43 ± 1.02 55.34 ± 1.32
	100	pl	0 9	10	 283 ± 24	55.56 ± 0.47 55.70 ± 0.88
	105	pl	0 9	10	 280 ± 17	55.75 ± 0.75 56.17 ± 1.06
B1	80	នន	9	10	 234 ± 12	60.45 ± 0.85 61.10 ± 0.80
	85	នន	0	10	 224 ± 16	59.99 ± 1.88 62.23 ± 0.92
	06	SS	0	10	232 ± 17	60.23 ± 0.74 61.52 ± 0.54
	95	SS	0	10	 242 ± 28	60.27 ± 0.95 61.37 ± 0.58
	100	នន	0	10	230 ± 17	60.77 ± 0.59 61.65 ± 0.62
	105	SS	9	10	240 ± 17	60.56 ± 0.87 63.19 ± 3.70

		TAB	TABLE 20 - continued	ıtinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	80	pl	9	10	222 ± 22	59.08 ± 0.64 59.35 ± 0.46
	85	pl	0	10	236 ± 22	58.83 ± 2.94 60.18 ± 0.87
	06	pl	0 9	10	234 ± 20	59.55 ± 0.79 60.05 ± 1.17
	95	pl	0	10	 255 ± 24	59.14 ± 1.68 59.80 ± 2.01
	100	pl	0	10	 249 ± 20	59.91 ± 0.48 60.39 ± 1.38
	105	pl	0	10	 249 ± 16	59.32 ± 0.61 60.00 ± 0.37

		<u> </u>	T						-	
(50/50)	Valve Delivery (mg/actuation)	57.35 ± 1.07 58.50 ± 0.54	56.97 ± 0.64 57.92 ± 0.64	56.87 ± 0.87 57.99 ± 0.74	57.65 ± 1.16 58.46 ± 0.89	+++	57.83 ± 1.10 58.77 ± 0.88	56.73 ± 0.66 55.55 ± 3.81	56.13 ± 1.85 56.23 ± 0.77	++++
NT 7/GERS 1085 NT (50	Leak Rate (mg/yr)	 267 ± 15	273 ± 14	279 ± 24	267 ± 10	 265 ± 16	266 ± 11	284 ± 17	282 ± 23	267 ± 9
7 NT 7/G	N	10	10	10	10	10	10	10	10	10
TABLE 21 DFDA 1137	Time (Weeks)	9	0	0 9	0	9	0	0	0	09
YMER BLEND	Stem	ន	SS	ល	ន	ស	SS	pl	pl	pl
OLDED POI	Œ	80	85	06	95	100	105	80	85	90
COMPRESSION MOLDED POLYMER BLEND.	Formulation	A1								

	T					1				
	Valve Delivery (mg/actuation)	56.69 ± 0.73 57.21 ± 0.38	55.28 ± 3.52 56.98 ± 0.55	57.15 ± 0.41 57.06 ± 0.62	61.83 ± 0.93 63.37 ± 0.87	60.98 ± 0.78 62.90 ± 0.99	61.80 ± 0.85 63.12 ± 0.94	61.94 ± 1.11 63.26 ± 0.86	61.94 ± 0.95 62.99 ± 0.97	62.61 ± 0.96 63.70 ± 0.78
	Leak Rate (mg/yr)	285 ± 29	269 ± 8	271 ± 12	 206 ± 9	 206 ± 17	 196 ± 11	 205 ± 11	 201 ± 13	192 ± 12
continued	. Z	10	10	10	10	10	10	10	10	10
21 -	Time (Weeks)	0	0	0	0	OΨ	0	6	0	0
TABLE	Stem	pl	pl	pl	88	88	ស្ល	SS	SS	SS
	ID	95	100	105	80	85	06	95	100	105
	Formulation				В1					

		TAB	TABLE 21 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/ <u>y</u> r)	Valve Delivery (mg/actuation)
	80	pl	0	10	210 ± 19	60.39 ± 0.60 61.08 ± 0.71
	85	pl	9	10	211 ± 11	59.80 ± 0.38 61.44 ± 1.31
	06	pl	.0	10	202 ± 10	61.52 ± 0.58 61.89 ± 0.63
	95	pl	9	10	193 ± 8	55.62 ± 17.44 61.96 ± 0.94
	100	pl	0	10	 202 ± 13	61.30 ± 0.52 62.18 ± 0.56
	105	pl	0	10	 203 ± 15	61.53 ± 0.86 61.68 ± 0.75

5					-					
(75/25)	Valve Delivery (mg/actuation)	57.92 ± 1.25 58.18 ± 0.84	58.31 ± 0.90 58.85 ± 0.80	58.01 ± 0.58 58.85 ± 0.80	57.93 ± 0.84 58.86 ± 0.77	57.23 ± 1.01 58.20 ± 0.94	58.07 ± 1.13 58.61 ± 1.07	57.07 ± 1.02 57.31 ± 0.62	57.39 ± 0.39 57.83 ± 0.53	57.14 ± 0.51 57.45 ± 0.81
NT 7/GERS 1085 NT (75	Leak Rate (mg/yr)	 374 ± 24	385 ± 27	332 ± 16	314 ± 28	294 ± 16	324 ± 19	392 ± 20	 380 ± 41	340 ± 27
	Z	10	1.0	10	10	10	10	10	10	10
TABLE 22 DFDA 1137	Time (Weeks)	0	9	0	9	9	0 9	0	0 9	0 9
YMER BLEND.	Stem	ល	ល	ន	ន	នន	ល	pl	þĵ	pl
OLDED POL	ID	80	85	06	95	100	105	80	38	06
COMPRESSION MOLDED POLYMER BLEND.	Formulation	A1								

		TAE	TABLE 22 - CO	continued		
Formulation	ID	Stem	Time (Weeks)	z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	95	pl	0 .6	10	 299 ± 16	57.54 ± 0.50 57.44 ± 0.57
	100	pl	9	10	309 ± 13	56.95 ± 0.71 57.38 ± 2.62
	105	pl	0	10	331 ± 29	56.13 ± 1.71 56.78 ± 0.80
81	80	ស	9	10	 205 ± 13	61.92 ± 0.77 63.21 ± 0.61
	85	ល	0	10	 201 ± 6	61.81 ± 0.52 63.52 ± 0.57
	90	SS	0	10	 201 ± 11	61.80 ± 1.23 63.63 ± 1.68
	95	SS	0	10	 201 ± 15	61.86 ± 0.86 63.32 ± 0.98
	100	SS	0	10	209 ± 23	62.16 ± 0.94 63.64 ± 0.97
	105	SS	0	10	204 ± 11	62.46 ± 0.83 63.39 ± 1.11

		TAB	TABLE 22 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/ <u>y</u> r)	Valve Delivery (mg/actuation)
	80	pl	0	10	 199 ± 11	60.75 ± 0.62 61.62 ± 0.64
	85	pl	9	10	212 ± 16	60.93 ± 0.50 62.08 ± 0.72
	90	pl	0	10	 205 ± 14	60.44 ± 1.84 62.48 ± 1.21
	95	pl	0	10	205 ± 7	61.06 ± 0.47 62.12 ± 0.95
	100	pl	0	10	210 ± 27	60.49 ± 0.68 61.41 ± 0.67
	105	ľď	0 9	10	201 ± 13	60.54 ± 2.61 61.96 ± 0.74

			_							
(23.2/69.8/7.0)	Valve Delivery (mg/actuation)	59.26 ± 1.00 59.82 ± 1.06	59.19 ± 0.85 60.39 ± 0.83	60.44 ± 1.07 62.03 ± 0.70	59.71 ± 1.90 61.78 ± 0.57	59.61 ± 0.84 61.31 ± 0.84	59.98 ± 1.21 61.49 ± 1.06	57.71 ± 0.70 57.54 ± 0.63	57.73 ± 0.54 57.56 ± 0.33	58.04 ± 0.78 58.46 ± 0.64
23 NT 7/GERS 1085 NT/TALC	Leak Rate (mg/yr)	296 ± 37	265 ± 31	 278 ± 34	313 ± 43	303 ± 40	 311 ± 53	300 ± 48	264 ± 29	 287 ± 33
7/GERS	z	10	10	10	10	10	10	10	10	10
TABLE 23 DFDA 1137 NT	Time (Weeks)	0 9	0 9	0	0	0	0 9	0	0	9
	Stem	ន	SS	SS	SS	SS	ល	pl	pl	pl
D POLYMER	ID	80	85	90	95	100	105	80	85	06
COMPRESSION MOLDED POLYMER BLEND.	Formulation	A2								·

		TABLE	23 -	continued		
Formulation	T.	Stem	Time (Weeks)	N	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	95	pl	0	10	282 ± 22	58.24 ± 0.70 58.79 ± 0.59
	100	pl	0 9	10	310 ± 43	57.80 ± 0.44 59.33 ± 1.45
	105	þĵ	0	10	6€ ∓ 99£	58.30 ± 0.61 59.16 ± 0.44
B2	80	ល	9	10	 194 ± 6	61.80 ± 1.00 not measured
	85	Ω Ω	0 9	10	185 ± 16	61.94 ± 0.98 64.04 ± 0.69
	06	ស ស	0 9	10	 206 ± 28	61.40 ± 2.70 65.21 ± 0.88
	95	SS	0 	10	196 ± 15	62.82 ± 1.03 65.31 ± 0.81
	100	ស	9	10	218 ± 35	60.04 ± 6.25 65.37 ± 0.67
-	105	ល	9	10	215 ± 36	63.57 ± 1.54 65.14 ± 0.77

		TAB	TABLE 23 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/ <u>yr</u>)	Valve Delivery (mg/actuation)
	80	pl	0	10	 221 ± 41	60.74 ± 0.73 61.69 ± 0.65
	85	pl	0	10	188 ± 7	60.69 ± 0.79 61.99 ± 0.72
	90	pl	0	10	199 ± 13	61.33 ± 0.88 62.34 ± 0.53
	95	pl	0	10	212 ± 18	61.13 ± 0.72 63.36 ± 1.23
	100	pl	0	10	 210 ± 24	60.71 ± 1.08 64.28 ± 2.53
	105	pl	9	10	205 ± 33	61.28 ± 0.44 64.10 ± 1.27

(46.5/7.0)	Valve Delivery (mg/actuation)	57.80 ± 3.05 61.25 ± 0.81	60.00 ± 0.91 61.72 ± 0.94	60.37 ± 0.90 62.18 ± 0.74	59.91 ± 0.95 61.84 ± 0.92	+++	60.59 ± 1.22 61.76 ± 0.72	58.27 ± 0.56 57.59 ± 2.34	58.17 ± 1.13 59.03 ± 0.37	57.39 ± 2.30
4 NT 7/GERS 1085 NT/ TALC (46.5/46.5/7.0)	Leak Rate Val	9	229 ± 15 6:	266 ± 34 63	266 ± 26 61	231 ± 30 61.	60 293 ± 38 63	248 ± 24 57.	58 238 ± 21 59	244 + 19
NT 7/GERS 1085	N Le	10 2	10 2	10 2	10 2	10 2	10	10	10 2	10
TABLE 24 DFDA 1137	Time (Weeks)	0 9	9	0 9	0	3	9	0 9	0 9	0
POLYMER BLEND.	Stem	SS	ល	SS	ល	ល	ល	pl	pl	þĵ
LDED POLYN	ID	80	85	06	95	100	105	80	85	06
COMPRESSION MOLDED	Formulation	A2								

		TABLE	24 -	continued		
Formulation	ID	Stem	Time (Weeks)	z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	95	pl	0	10	 280 ± 40	58.69 ± 0.61 59.20 ± 0.85
	100	τď	9	10	297 ± 30	58.53 ± 0.52 59.55 ± 1.40
	105	pl	0	10	280 ± 30	58.88 ± 0.30 60.89 ± 2.31
B2	80	ល	9	10	 186 ± 20	64.01 ± 1.29 65.56 ± 0.70
	85	និ	9	10	 191 ± 9	63.40 ± 0.71 65.8 ± 0.92
	06	ន	9	10	 200 ± 16	63.40 ± 1.26 65.74 ± 1.21
	95	SS	0	10	 197 ± 9	63.07 ± 0.74 65.83 ± 0.74
	100	SS	0	10	 194 ± 9	63.02 ± 1.44 65.51 ± 1.62
	105	SS	9	10	 185 ± 10	63.98 ± 0.64 65.71 ± 0.98

		TAB	TABLE 24 - cor	- continued			
Formulation	ID	Stem	Time (Weeks)	N	Leak Rate (mg/ <u>y</u> r)	Valve Delivery (mg/actuation)	
	80	pl	0	10	 200 ± 19	61.25 ± 0.50 62.19 ± 0.42	
	85	pl	0 .	10	197 ± 14	61.69 ± 0.62 62.58 ± 1.28	
	06	pl	0	10	 200 ± 12	61.43 ± 1.51 62.77 ± 0.88	
	. 36	pl	9	10	 208 ± 14	61.50 ± 0.57 63.75 ± 0.91	
	100	: pl	0	10	203 ± 10	62.26 ± 0.54 64.25 ± 2.12	
	105	p].	0 6	10	 188 ± 13	61.94 ± 0.58 63.39 ± 0.64	

				l l		1	1		1	T
69.8/23.2/7.0)	Valve Delivery (mg/actuation)	60.31 ± 0.91 62.18 ± 0.90	60.53 ± 1.09 62.01 ± 0.70	59.66 ± 1.41 62.05 ± 0.74	60.06 ± 1.36 62.10 ± 0.77	61.05 ± 1.03 61.70 ± 0.83	60.86 ± 0.93 61.50 ± 1.01	58.44 ± 0.54 58.22 ± 1.62	58.73 ± 0.44 59.01 ± 0.56	58.79 ± 0.66 59.52 ± 0.61
7/GERS 1085 NT/TALC (69.8/23.2/7.0)	Leak Rate (mg/yr)	330 ± 53	422 ± 197	302 ± 59	333 ± 74	331 ± 42	297 ± 41	 288 ± 41	303 ± 30	275 ± 29
<u>5</u> NT 7/GERS	N	10	10	10	10	10	10	10	10	10
TABLE 25 DFDA 1137 N	Time (Weeks)	0 6	0	0	9	0	9	0	9	0
POLYMER BLEND.	Stem	ន	ល	SS	SS	នន	SS	pl	pl	pl
ED POLYME	QI	80	85	90	95	100	105	80	85	06
COMPRESSION MOLDED	Formulation	A2								

		TABLE	25 -	continued		
Formulation	ΩI	Stem	Time (Weeks)	z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	36	pl	0	10	322 ± 59	58.87 ± 1.21 60.48 ± 1.39
	100	pl	0	10	306 ± 33	59.35 ± 0.66 61.10 ± 1.59
	105	pl	0	10	302 ± 38	59.24 ± 0.59 58.71 ± 3.32
B2	8.0	ស	0 9	10	230 ± 69	64.24 ± 0.51 65.83 ± 0.56
	85	SS	09	10	 231 ± 145	63.78 ± 1.10 65.94 ± 1.09
	06	SS	9	10	201 ± 17	64.50 ± 1.30 66.09 ± 0.66
	95	SS	9	10	204 ± 19	62.51 ± 1.58 66.05 ± 1.10
	100	នន	9	10	202 ± 27	64.14 ± 0.81 65.86 ± 0.92
	105	SS	0 9	10	219 ± 70	64.41 ± 0.92 66.38 ± 0.96

		TA	TABLE 25- continued	tinued		
Formulation	ΙD	Stem	Time (Weeks)	N	Leak Rate (mg/ <u>yr</u>)	Valve Delivery (mg/actuation)
	80	pl	0	10	199 ± 10	62.09 ± 0.49 62.50 ± 0.59
	85	pl	9	10	 199 ± 16	61.77 ± 1.82 64.04 ± 1.66
	90	pl	0	10	202 ± 17	62.47 ± 0.66 63.89 ± 1.54
	95	p1	0	10	198 ± 13	62.50 ± 0.52 63.87 ± 1.27
	100	pl	0	10	 206 ± 18	62.67 ± 0.64 66.47 ± 4.74
	105	pl	9	10	 194 ± 12	62.35 ± 0.49 63.83 ± 0.92

The results in TABLES 20-25 show that the indicated blends are suitable seal materials for use with metered dose inhalers containing the indicated formulations. Moreover, the data indicate that blends in all proportions would be suitable.

Diaphragms of the invention were prepared from ATTANE^M 4602 polyolefin and ATTANE^M 4701 polyolefin and tested with the formulations indicated in TABLE 26 and TABLE 27 below, respectively:

•									
	Valve Delivery (mg/actuation)	62.21 ± 0.76 61.43 ± 1.65	62.37 ± 1.64 61.31 ± 1.07	62.17 ± 0.65 61.45 ± 1.90	61.71 ± 0.47 60.41 ± 4.32	61.46 ± 1.04 54.14 ± 16.75	61.78 ± 1.17 61.58 ± 0.96	59.41 ± 0.34 58.38 ± 0.58	58.74 ± 1.70 56.81 ± 5.49
OLYOLEFIN	Leak Rate (mg/yr)	 1442 ± 595	1611 ± 499	 1917 ± 1245	1410 ± 720	1177 ± 644	1824 ± 2007	285 ± 23	 390 ± 216
* 4602 PC	N	10	10	10	10	10	10	10	10
DED ATTANE	Time (Weeks)	0	0	9	0	9	9	0	0
COMPRESSION MOLDED ATTANE" 4602 POLYOLEFIN	Stem	ល	ល	ល	ន	នន	នន	pl	pl
COMP	ID	80	85	06	95	100	105	80	85
	Formulation	А3							·

		TABLE	26 -	continued		
Formulation	ID	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	90	pl	0	10	 316 ± 46	59.42 ± 0.62 58.40 ± 1.08
	95	pl	0	10	440 ± 430	59.59 ± 0.62 56.25 ± 4.51
	100	рl	9	10	 328 ± 91	59.89 ± 0.64 59.84 ± 1.74
	105	pl	0 9	10	 419 ± 218	59.38 ± 1.03 60.04 ± 2.83
B2	80	ល	0 9	10	 802 ± 1034	66.53 ± 0.92 67.86 ± 0.81
	85	<u>ທ</u>	0 9	10	 812 ± 425	66.14 ± 0.55 66.70 ± 0.72
	90	SS	0 9	10	812 ± 644	66.18 ± 1.18 66.61 ± 0.85
	95	SS	9	10	925 ± 712	65.97 ± 1.11 66.76 ± 0.80
·	100	SS	0 9	10	1067 ± 1137	66.02 ± 0.98 66.36 ± 1.03

		TAB	TABLE 26 - CO	continued		
Formulation	ΩI	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	105	SS	0	10	 1169 ± 1462	66.29 ± 0.88 66.39 ± 1.96
	80	pl	9	10	 163 ± 17	63.92 ± 0.40 63.64 ± 0.95
	85	pl	0	10	TE ‡ 28T	63.72 ± 0.95 63.93 ± 0.70
	06	pl	0	10	 189 ± 42	64.26 ± 3.81 64.36 ± 0.82
	95	pl	0	10	 166 ± 13	63.57 ± 1.13 64.99 ± 3.07
	100	pl	0	10	198 ± 38	63.55 ± 1.47 65.23 ± 2.72
	105	pl	9	10	2334 ± 3940	65.46 ± 2.42 74.03 ± 33.09

	Valve Delivery (mg/actuation)	61.73 ± 0.81 60.04 ± 3.46	62.27 ± 0.88 61.84 ± 0.71	62.37 ± 0.69 61.98 ± 0.46	61.81 ± 0.63 61.09 ± 1.57	61.79 ± 0.79 61.35 ± 0.94	61.21 ± 0.85 60.67 ± 0.92	59.51 ± 0.85 58.45 ± 0.84	59.43 ± 1.31 57.03 ± 2.39	59.62 ± 0.65 58.96 ± 0.62	59.50 ± 0.69 58.77 ± 1.03
COMPRESSION MOLDED ATTANET 4701 POLYOLEFIN	Leak Rate (mg/yr)	2377 ± 394	2263 ± 1534	1817 ± 793	2447 ± 2861	2441 ± 1081	 1480 ± 867	356 ± 71	 294 ± 21	322 ± 59	297 ± 26
LTANE" 4	z	10	10	10	10	10	10	10	10	1.0	10
N MOLDED A	Time (Weeks)	0	9	9	9	9	9	9	9	9	0
11	Stem	SS	SS	នន	SS	SS	នន	pl	pl	pl	pl
<u>TABLE 27 - </u>	ID	80	85	06	95	100	105	. 80	85	90	95
E	Formulation	A3									

		TAE	TABLE 27 - CO	continued		
Formulation	ID	Stem	Time (Weeks)	X	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	100	pl	0	10	326 ± 33	57.92 ± 2.91 58.49 ± 0.99
	105	pl	0	10	1093 ± 1193	57.30 ± 5.32 58.23 ± 0.71
B2	80	SS	0	10	 617 ± 382	66.58 ± 1.01 67.42 ± 1.08
	85	ល	0	10	 745 ± 610	67.25 ± 1.56 67.40 ± 0.72
	90	ល	9	10	716 ± 489	66.75 ± 1.01 67.44 ± 1.01
	95	SS	0	10	797 ± 602	66.86 ± 0.74 67.05 ± 0.76
	100	នន	0	10	 1145 ± 1080	66.36 ± 0.66 67.06 ± 0.41
	105	SS	0	10	 1020 ± 731	66.18 ± 0.98 66.33 ± 0.90
	80	pl	9	10	 176 ± 20	64.11 ± 0.44 63.87 ± 0.74

		TAB	TABLE 27 - continued	ntinued		
Formulation	ID	Stem	Time (Weeks)	Z	Leak Rate (mg/yr)	Valve Delivery (mg/actuation)
	85	pl	0	10	175 ± 17	63.45 ± 1.06 63.97 ± 0.79
	06	pl	0	10	177 ± 16	64.14 ± 0.47 63.40 ± 3.13
	95	pl	0 9	10	 200 ± 68	63.17 ± 2.12 64.89 ± 1.22
	100	pl	6	10	 197 ± 11	63.96 ± 0.82 64.09 ± 0.78
	105	Įď	0	10	254 ± 174	63.46 ± 0.58 64.50 ± 1.25

The results in TABLES 26 and 27 show that diaphragms of these materials are suitable but perform notably better with the indicated albuterol sulfate and beclomethasone dipropionate formulations when used with 5 a plastic valve stem.

For comparative purposes, diaphragms were prepared from "Buna" rubber and from butyl rubber, both materials being commonly used in commercially available metered dose inhalers. These diaphragms were tested with formulations as indicated in TABLES 28 and 29 below:

	e Valve Delivery (mg/actuation)	56 ± 1	51.11 ± 1.33	82 ± 1	2.81 ±	52.97 ± 1.	4.19 ±	$3.05 \pm 1.$	51.88	54.14 ± 1.	3.88 ± 1.	53.78	54.05 ± 1.	.62 \pm 0.	49.00 ± 1.1	51.02 ± 0.7	.32 ±	52.53 ± 2.	53.71 ± 0.	$1.22 \pm 0.$	49.94 ± 1.3	51.00 ± 0.4	$1.27 \pm 0.$	12 50.57 ± 0.62	$51.13 \pm 0.$
	Leak Rate (mg/yr)	-	+1 9	377 ± 14		4	92 ± 1	=	345 ± 12	+1 9	1	345 ± 16	+ı		312 ± 18	395 ± 160		Ŋ	+1	-	+1	378 ± 22	1	322 ± 1	+1
RUBBER	Z	20/12			20/12			20/12			20/12			20/12			20/12	•		20/12	•		20/12	•	
28 - BUNA	Time (Weeks)	0	4	12	0	4	12	0	4	12	0	4	12	0	4	12	0	4	12	0	4	12	0	4	12
TABLE	Stem	SS	i i		SS	1		SS			SS			D1	4		pl	4		p]	<u>.</u>		p]	!	
	ID	83)		88)		93) 		86			83			88			93			98		
	Formulation	AS)																						

			T	y					
	Valve Delivery (mq/actuation)	58.86 ± 2.59 57.98 ± 2.04 58.13 + 3.15	++++	9.12 + 2 8.72 + 3 8.92 + 3	8.74 ± 2 8.02 ± 2 0.59 + 4	92 ± 0. 45 ± 1. 62 ± 1.	6.31 ± 0.4.50 ± 3.	6.20 ± 0. 5.04 ± 0.	.67 ± 1. .16 ± 0. .24 ± 0.
	Leak Rate (mq/yr)	 174 ± 24 216 ± 16	1+1+1	+1+1	+1+1	+++	169 ± 25 218 ± 22	61 + 1	 156 ± 11 204 ± 11
RUBBER	Z	20/12	20/12	20/12	20/12	20/12	20/12	20/12	20/12
29 - BUTYL	Time (Weeks)	12	0 4 12	0 4 12	0 4 12	0 4 12	0 4 12	0 4 12	0 4 12
TABLE	Stem	ន	នន	នន	SS	pl	pl	pl	pl
	ID	83	88	93	98	83	88	93	86
	Formulation	A5			·				

The results in TABLES 28 and 29 show that, when used with the indicated formulations, "Buna" diaphragms generally exhibit leak rates higher than 300 mg/yr with generally acceptable valve delivery variability. The results also show that the butyl rubber diaphragms exhibit acceptable leak rates when used with the indicated formulations but valve delivery variability is not acceptable.

Diaphragms of the invention were prepared

10 from the materials set forth in TABLES 30 and 31 and
tested with the indicated formulations. In said

TABLES, Valve "A" indicates that the valve used was a
valve with a stainless steel valve stem, substantially
as described herein and illustrated in the Drawing.

15 Valve "B" indicates that the valve used was a 50 μ L SPRAYMISER aerosol valve (Neotechnic Engineering Ltd.).

227	N = 5	Valve Delivery	(mq/actuation)±SD	67.78 ± 0.51	+1	65.84 ± 1.14	66.08 ± 0.70	66.40 ± 4.30	68.34 ± 0.86	68.20 ± 1.02	+1	69.08 ± 1.32	+1	69.34 ± 0.89	68.94 ± 0.36	70.72 ± 0.52	+1	+1	69.46 ± 3.16	70.84 ± 1.23	69.78 ± 1.57	70.14 ± 2.10	69.76 ± 1.42
DIAPHRAGM PERFORMANCE WITH HFC-227	N = 10	Leak Rate	(mg/yr)±SD		13 ± 6	1	8 ± 8	-	12 ± 6		3 + 4		15 ± 6		6 ± 5		11 ± 3	1	32 ± 59	1 1 1	12 ± 8	-	5 ± 6
PERFORMAN		Time	(Weeks)	0	3	0	3	0	3	0	3	0	m	0	3	0	3	0	3	0	3	0	3
PHRAGM			Valve	A		Ø		A		В		Ą		B		A		Ø		K		В	
TABLE 30 - DIA	,	Diaphragm	Marerial	GERS 1085 NT				- 1	1085 NT			NT7	$\frac{\text{GERS 1085 NT}}{\text{Talc}} = \frac{46.5}{7.0}$			Attane 4602				Attane™ 4701			
		Form: 104:02	LOTHUTACTON	Д																			

<u>TABLE 31</u> Diaphragm Performance With HFC-227 Formulations

				N = 10	N = 5
			Time	Leak Rate	Valve Delivery
Formulation	Diaphragm	Valve	(Weeks)	(mg/yr)+SD	(mg/actuation)+SD
A7	GERS 1085 NT	A	0	! !	68.27 ± 6.23
			*	47 ± 9	40.60 ± 28.88
		В	0		75.42 ± 1.64
			*	41 ± 9	75.60 ± 0.91
	DFDA 1137 NT7 = 50	Ą	0		75.88 ± 3.74
	1085 NT		*	66 ± 56	+1
		В	0	1	78.30 ± 1.13
			*	37 ± 9	77.92 ± 0.25
	DFDA 1137 NT7 46.5	A	0		74.84 ± 1.62
	11		*	50 ± 14	+1
		В	0	!	79.70 ± 4.78
-			*	37 ± 9	78.33 ± 0.71
	Attane™ 4602	Ą	0		79.10 ± 4.46
			*	7047 ± 4844	80.00 ± 1.95
		В	0	-	78.60 ± 0.83
			*	60 ± 55	58.82 ± 28.9
	Attane™ 4701	Ą	0		77.44 ± 2.67
			*	43 ± 8	77.48 ± 12.02
		В	0	CON CITY 6420	76.30 ± 3.50
			*	30 ± 15	66.60 ± 13.02
		•			100

- 103 -

The results in TABLES 30 and 31 indicate that these diaphragms of the invention function as seal materials for use in the dynamic pressure seal of a metered dose inhaler containing a formulation that 5 comprises HFC-227. Furthermore, these data demonstrate the dramatic difference in valve delivery variability depending on the presence of a small amount of ethanol as a formulation component and the nature of the drug substance. The difference between valve A and valve B 10 is especially clear in TABLE 31 where Valve A affords unsatisfactory valve delivery variability while valve B exhibits very low variability. Within a valve type, for example valve B, the material from which the diaphragm is constructed also has an important effect, 15 which is illustrated by the results for GERS 1085 NT and the several blends on one hand, and ATTANE m 4602 and ATTANE™ on the other hand.

The Claimed Invention Is:

- 1. A device for delivering an aerosol, comprising: a valve stem, a diaphragm having walls defining a diaphragm aperture, and a casing member having walls defining a casing aperture, wherein the valve stem passes through the diaphragm aperture and the casing aperture and is in slidable sealing engagement with the diaphragm aperture, and wherein the diaphragm is in sealing engagement with the casing member, the diaphragm material comprising: a thermoplastic elastomer comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, and 1-octene.
 - 2. A device according to Claim 1, wherein the sole comonomer is 1-butene.

- 3. A device according to Claim 1, wherein the sole comonomer is 1-hexene.
- 4. A device according to Claim 1, wherein 25 the sole comonomer is 1-octene.
- 5. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 91 mole percent ethylene and about 9 mole percent 30 1-butene.
- 6. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 88 mole percent ethylene and about 12 mole 35 percent 1-butene.

- 105 -

7. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 80 mole percent ethylene and about 20 mole percent 1-butene.

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8. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 90 mole percent ethylene and about 10 mole percent 1-butene.

10

9. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 92 mole percent ethylene and about 8 mole percent 1-butene.

15

10. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 90 mole percent ethylene and about 10 mole percent 1-octene.

20

11. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 92 mole percent ethylene and about 8 percent 1-octene.

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12. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 95 mole percent ethylene, about 1 mole percent 1-butene, and about 4 mole percent 1-hexene.

30

13. A device according to Claim 1, wherein the thermoplastic elastomer comprises a copolymer of about 94 mole percent ethylene, about 1 mole percent 1-butene, and about 5 mole percent 1-octene.

- 14. A device according to Claim 1, wherein the thermoplastic elastomer is a thermoplastic polymer blend comprising at least two thermoplastic copolymers, each comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, and 1-octene.
- 10 15. A device according to Claim 14, wherein the sole comonomer in each of the copolymers is 1-butene.
- 16. A device according to Claim 14,
 15 wherein the thermoplastic polymer blend comprises (i) a copolymer of about 91 mole percent ethylene and about 9 mole percent 1-butene, and (ii) a copolymer of about 80 mole percent ethylene and about 20 mole percent 1-butene.

17. A device according to Claim 16, wherein the thermoplastic polymer blend comprises one part by weight of component (i) and about 0.25 to about 4 parts by weight of component (ii).

25

18. A device according to Claim 1, further comprising: a tank seal having walls defining a tank seal aperture, and a metering tank of a predetermined volume and having an inlet end, an inlet aperture, and 30 an outlet end, wherein the outlet end is in sealing engagement with the diaphragm, the valve stem passes through the inlet aperture and the tank seal aperture and is in slidable engagement with the tank seal aperture, and the tank seal is in sealing engagement with the inlet end of the metering tank, and wherein the valve stem is movable between an extended closed position, in which the inlet end of the metering tank is open and the outlet end is closed, and a compressed

- 107 -

open position in which the inlet end of the metering tank is substantially sealed and the outlet end is open to the ambient atmosphere.

- 5 19. A device according to Claim 1, wherein the casing member defines a formulation chamber.
- 20. A device according to Claim 19, wherein the formulation chamber contains an aerosol 10 formulation comprising 1,1,1,2-tetrafluoroethane, 1,1,1,2,3,3,3-heptafluoropropane, or a mixture thereof, in an amount effective to function as a propellant.
- 21. A device according to Claim 20,

 15 wherein the formulation is a pharmaceutical formulation comprising 1,1,1,2-tetrafluoroethane, 1,1,1,2,3,3,3-heptafluoropropane, or a mixture thereof, in an amount effective to function as an aerosol propellant, and a drug in an amount sufficient to provide a predetermined number of therapeutically effective doses for inhalation.
 - 22. A device according to Claim 21, wherein the drug is a bronchodilator or a steroid.
- 23. A device according to Claim 21, wherein the drug is albuterol sulfate.
- 24. A device according to Claim 21, 30 wherein the drug is beclomethasone dipropionate.
 - 25. A device according to Claim 21, wherein the drug is pirbuterol acetate.
- 35 26. A device according to Claim 20, wherein the formulation further comprises ethanol.

- 27. A device according to Claim 26, wherein the formulation further comprises oleic acid.
- 5 member for minimizing and/or preventing escape of formulation components from a device for delivering an aerosol, wherein the sealing member comprises a thermoplastic elastomer comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, and 1-octene.
- 29. A sealing member according to Claim
 15 28, wherein the elastomer comprises about 91 mole
 percent ethylene and about 9 mole percent 1-butene,
 wherein the respective monomer units are substantially
 randomly distributed in the copolymer.
- 28, wherein the elastomer comprises: a copolymer of about 88 mole percent ethylene and about 12 mole percent 1-butene.
- 25 31. A sealing member according to Claim 28, wherein the sole comonomer is 1-butene.
 - 32. A sealing member according to Claim 28, wherein the sole comonomer is 1-hexene.
 - 33. A sealing member according to Claim 28, wherein the sole comonomer is 1-octene.
- 34. A sealing member according to Claim
 35 28, wherein the thermoplastic elastomer comprises a
 copolymer of about 80 mole percent ethylene and about
 20 mole percent 1-butene.

35. A sealing member according to Claim 28, wherein the thermoplastic elastomer comprises a copolymer of about 90 mole percent ethylene and about 10 mole percent 1-butene.

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36. A sealing member according to Claim 28, wherein the thermoplastic elastomer comprises a copolymer of about 92 mole percent ethylene and about 8 mole percent 1-butene.

10

37. A sealing member according to Claim 28, wherein the thermoplastic elastomer comprises a copolymer of about 90 mole percent ethylene and about 10 mole percent 1-octene.

15

38. A sealing member according to Claim 28, wherein the thermoplastic elastomer comprises a copolymer of about 92 mole percent ethylene and about 8 percent 1-octene.

- 39. A sealing member according to Claim 28, wherein the thermoplastic elastomer comprises a copolymer of about 95 mole percent ethylene, about 1 mole percent 1-butene, and about 4 mole percent 1-25 hexene.
- 40. A sealing member according to Claim 28, wherein the thermoplastic elastomer comprises a copolymer of about 94 mole percent ethylene, about 1 mole percent 1-butene, and about 5 mole percent 1-octene.
- 41. A sealing member according to Claim 28, wherein the thermoplastic elastomer is a thermoplastic polymer blend comprising at least two thermoplastic copolymers, each comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20 mole percent of one or

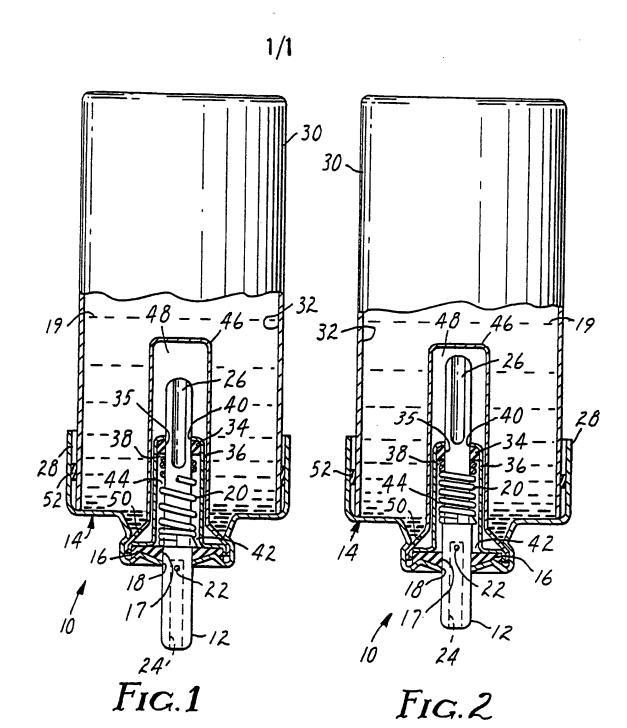
more comomoners selected from the group consisting of 1-butene, 1-hexene, and 1-octene.

- 42. A sealing member according to Claim 5 41, wherein the sole comonomer in each of the copolymers is 1-butene.
- 41. A sealing member according to Claim
 41, wherein the thermoplastic polymer blend comprises
 10 (i) a copolymer of about 91 mole percent ethylene and
 about 9 mole percent 1-butene and (ii) a copolymer of
 about 80 mole percent ethylene and about 20 mole
 percent 1-butene.
- 44. A sealing member according to Claim
 43, wherein the thermoplastic polymer blend comprises
 one part by weight of component (i) and about 0.25 to
 about 4 parts by weight of component (ii).
- 20 45. A sealing member according to Claim 28 further comprising talc.
 - 46. A sealing member according to Claim 28, in the form of a diaphragm
 - 47. A sealing member according to Claim 28, in the form of an O-ring.
- 48. A sealing member according to Claim 30 28, in the form of a gasket.
 - 49. A sealing member according to Claim 28, in the form of a tank seal.
- 35 50. A thermoplastic polymer blend comprising at least two thermoplastic copolymers, each comprising a copolymer of about 80 to about 95 mole percent ethylene and a total of about 5 to about 20

- 111 -

mole percent of one or more comonomers selected from the group consisting of 1-butene, 1-hexene, and 1octene.

- 51. A polymer blend according to Claim 50, wherein the sole comonomer in each copolymer is 1-butene.
- 52. A polymer blend according to Claim 50, comprising (i) a copolymer of about 91 mole percent ethylene and about 9 mole percent 1-butene and (ii) a copolymer of about 80 mole percent ethylene and about 20 mole percent 1-butene.
- 53. A polymer blend according to Claim 52, comprising one part by weight of component (i) and about 0.25 to about 4 parts by weight of component (ii).
- 54. A polymer blend according to Claim 50 in the form of a sealing member.
 - 55. A sealing member according to Claim 54 in the form of a diaphragm, an 0-ring, or a gasket.
 - 56. A method of sealing a chamber with a sealing member, comprising the step of sealing said chamber with a sealing member according to Claim 41.



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